

(19) World Intellectual Property Organization
International Bureau



(43) International Publication Date
13 December 2001 (13.12.2001)

PCT

(10) International Publication Number
WO 01/93704 A1

(51) International Patent Classification⁷: **A23N 7/00**

(21) International Application Number: PCT/IE01/00076

(22) International Filing Date: 5 June 2001 (05.06.2001)

(25) Filing Language: English

(26) Publication Language: English

(30) Priority Data:
2000/0456 6 June 2000 (06.06.2000) IE

(71) Applicant (for all designated States except US): **OSENEY LIMITED** [IE/IE]; Unit 2005, City West Business Campus, Naas Road, Dublin 24 (IE).

(72) Inventor; and

(75) Inventor/Applicant (for US only): **BRODERICK, Michael** [IE/IE]; Pollerton Big, County Carlow (IE).

(74) Agents: **WALSH, Michael, Joseph** et al.; Tomkins & Co., 5 Dartmouth Road, Dublin 6 (IE).

(81) Designated States (national): AE, AG, AL, AM, AT, AT (utility model), AU, AZ, BA, BB, BG, BR, BY, BZ, CA,

CH, CN, CO, CR, CU, CZ, CZ (utility model), DE, DE (utility model), DK, DK (utility model), DM, DZ, EC, EE, EE (utility model), ES, FI, FI (utility model), GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MA, MD, MG, MK, MN, MW, MX, MZ, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, SK (utility model), SL, TJ, TM, TR, TT, TZ, UA, UG, US, UZ, VN, YU, ZA, ZW.

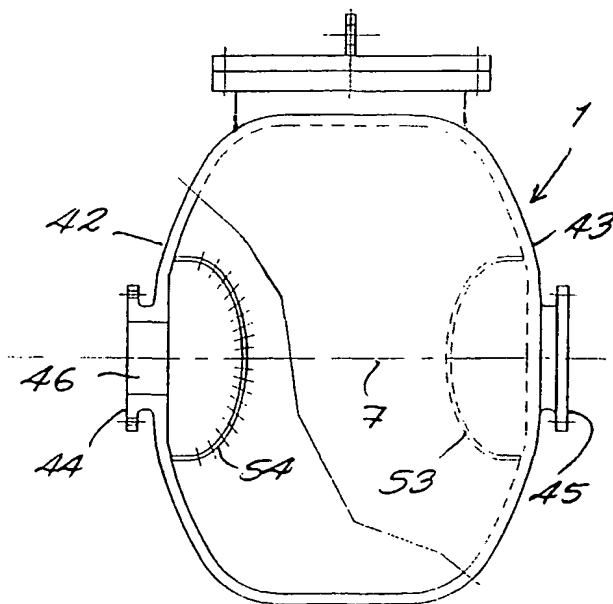
(84) Designated States (regional): ARIPO patent (GH, GM, KE, LS, MW, MZ, SD, SL, SZ, TZ, UG, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE, TR), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, GW, ML, MR, NE, SN, TD, TG).

Published:

- with international search report
- before the expiration of the time limit for amending the claims and to be republished in the event of receipt of amendments

For two-letter codes and other abbreviations, refer to the "Guidance Notes on Codes and Abbreviations" appearing at the beginning of each regular issue of the PCT Gazette.

(54) Title: STEAM PEELING PROCESSING SYSTEM



(57) Abstract: A pressure vessel (1) for steam treatment of product to be peeled in a steam peeling system has substantially the shape of a sphere with opposed flattened side surfaces. The pressure vessel (1) is rotatable and has at least one internal lifting feature (51a, 51b, 51c) for entraining and raising product relative to the axis of rotation of the pressure vessel (1) during rotation of the pressure vessel (1). The pressure vessel (1) also at least one internal region (53) which is closed-off against ingress of steam during product treatment, said region (53) defining a steam saver. The pressure vessel (1) may be incorporated in a product treatment system also including a batcher for delivery of product to be peeled. The system may provide for accelerated pressure drop on completion of a peeling operation, as well as including arrangements to minimise release of entrained solid matter and/or odours in exhaust steam. A control system enables unproductive displacement of the pressure vessel to be minimised.

WO 01/93704 A1

Title

STEAM PEELING PROCESSING SYSTEM

5 . Field of the Invention**Background to the Invention**

10 This invention relates to processing systems, in particular systems for the processing or treatment of food products. More specifically, the invention relates to steam peeling. The invention is especially directed to steam peeling systems, more particularly steam peeling apparatus including a steam peeler pressure vessel. The invention further relates to pressure relief or reduction arrangements for steam exhaust from a steam peeler pressure vessel, as well as arrangements for environmental
15 treatment of steam exhaust or discharge from a steam peeler pressure vessel and control systems for processing systems including steam peelers.

Description of the prior art

20 A first prior art steam peeler is shown in Figure 1, in an initial product loaded disposition, in which a generally cylindrical pressure vessel 101 is oriented with its axis at an oblique upward angle relative to the horizontal, for loading 102 of product 103 through the mouth 104 of the vessel 101 into an internal cage 119 rotatably mounted within vessel 101. Deaeration is then effected, the pressure vessel
25 101 is closed, and steam is blown in 105. The pressure vessel 101 is then rotated about an axis perpendicular to the plane of the paper into a disposition in which its axis of symmetry extends substantially horizontally and in the plane of the paper, at which stage the cage 119 is rotated within the vessel 101 about that axis of symmetry to effect the required peeling action while the vessel 101 remains charged with steam
30 under pressure. The pressure within the vessel 101 is then relieved by rapid discharge of the steam, so that the peel is detached from the product, following which

pivoting of the pressure vessel 101 about the axis perpendicular to the plane of the paper is again effected, to bring the mouth 104 of the vessel 101 into a downward disposition in which the axis of symmetry of the vessel 101 is oriented at an acute angle with respect to the horizontal, but below the horizontal as compared with the disposition shown in the drawing, at which stage the product 103 is discharged from the pressure vessel 101. The structure is technically complex, because of the diversity of pivoting and rotational movements required, together with the necessity to be able to admit and discharge steam under pressure at various different stages in the sequence of movements, as well as closing the vessel 101 and maintaining it in a sealed condition during the operational cycles.

In Figure 2, a second form of rotatable steam peeling pressure vessel 201 is shown. In this arrangement, the vessel 201 is rotatable about an axis again perpendicular to the plane of the paper and is initially oriented in a disposition in which its axis of general symmetry 208 is disposed vertically upwards for product charging, 202 through mouth 204, as shown in the drawing. The loading and discharge opening 204 of the pressure vessel 201 is sealed by means of a door 206 which closes from the interior, thereby limiting the extent to which the pressure vessel 201 can be filled with product 203, in that the door 206 closing path of movement must be clear of product 203 during closing and opening movements. During steam peeling, rotation takes place by the pressure vessel 201 being turned about the axis perpendicular to the plane of the paper. By contrast with the arrangement of Figure 1, rotation of the pressure vessel 201 is provided only about one axis, rather than the two degree of freedom arrangement provided by the structure of Figure 1. There is no rotation about the axis of symmetry 208 of the pressure vessel 201. On completion of the pressurised steaming period, the vessel 201 is returned to the upright orientation shown in the drawing, pressure is released, and condensate may drain away at the base 211 of the pressure vessel 201 where the product is supported on a grid 213. When pressure is released, the door or inwardly opening lid 206 may also be opened, following which the pressure vessel 201 is inverted or substantially inverted for product 203 discharge. Disadvantages of the arrangement include the

necessity for the pressure vessel 201 to be restored to an orientation in an upward direction for opening and closing of the door 206, while also the necessity to provide for drain of condensate arises out of a relatively slow reduction in pressure being applied in the system of Figure 2, so that condensate forms within the pressure vessel 201, as compared with systems in which rapid flash or high-speed exhaust of the pressurised steam is provided, where formation of condensate within the pressure vessel is substantially minimised.

In the third prior art arrangement in which a rotating pressure vessel is used, as shown in Figure 3, the pressure vessel 301 is mounted for rotation about a substantially horizontal axis 307 extending in the plane of the paper of the drawing. The pressure vessel 301 is however mounted on this axis 307 in a skewed or canted manner, so that its general axis of symmetry 308 at all times defines an acute angle with respect to the axis 307 of rotation. Charging 302 of the pressure vessel 301 takes place in the manner previously described with the opening 304 of the pressure vessel 301 being upwardly directed, and discharge takes place when the pressure vessel 301 is turned so that the opening 304 is directed downwardly. When the pressure vessel 301 is loaded and sealed by closure of the vessel door, it is charged 305 with steam and is rotated about the horizontal axis 307, but remains in its canted or skewed disposition with respect to this axis 307 at all times. Again in this structure, there is no rotation about the axis of symmetry 308. Because of the canted or skewed arrangement of the pressure vessel 301, the construction is required to tolerate and withstand substantial out of balance forces during rotation of the pressure vessel 301, thereby necessitating a particularly robust and heavy supporting structure. Feed of product to the pressure vessel is effected by means of a weighing conveyor and associated ducting or a hopper arrangement 302, as applies also to the prior art apparatus of Figure 1 and may likewise be associated with the system of Figure 2. Exhaust is effected as indicated by reference numerals 314.

Figure 4 shows a first prior art arrangement using a static pressure vessel 401 which is equipped with a product inlet door 406 at the top 404 and a product

outlet door 409 at the bottom 411. Within the static pressure vessel 401, there is provided a continuously rotating agitator 412 and a condensate-separating grid 413. Fixed connections provide for steam supply 405 and exhaust 414 and for condensate discharge 415, all substantially automatically controlled during operation of the

5 system. After filling 402, product 403 to be peeled is held in the compartment 416 above the grid 413, while the agitator 412 keeps the product 403 moving, but without product damage. Separation of condensate, which forms in this system, is continuous throughout the steam exposure time, because of the rotational agitation which is effected about an axis 408 inclined relative to the horizontal. Condensate flows away

10 through the grid 413 and is evacuated by way of a condensate valve 415. At the end of the steaming time, the steam outlet valve 414 is opened for pressure drop to atmospheric. Discharge of product 403 through a door 417 in the grid 413 and subsequently through the product outlet port 411 is then effected. There is downstream transfer of product 403 by auger to a brush and belt skin removal

15 arrangement. The necessity for significant numbers of moving parts within the pressurised region, in particular three doors 406, 409 and 417, together with the need for pressure sealing of at least the drive 418 for the agitator 412 by way of a rotary joint or gland leads to a potentially significant maintenance requirement in a system of this kind, as well as high cost in construction.

20

A further peeling arrangement using a static pressure vessel is shown in Figure 5, in which product is charged 502 to a basket 519 which is located within a pressurisable region or dome 516. The basket 519 is shown in Figure 5 in a discharge or dump orientation and reference 502 indicates the direction of charging or loading

25 when the mouth of the basket 519 is directed upwards. The dome 516 is then sealed and charged with steam, while the basket 519 containing the product is rotated or turned within the dome 516, for exposure of the product to steam and immediate run-off of condensation. At the end of the steaming period, a large steam outlet provides for rapid fall in pressure to optimise bursting of the skin. As will be apparent

30 however from the drawing, the region 516 to be charged with steam is of significantly greater volume, to a multiple degree, than the region 519 of this system actually

containing product, so that the system of Figure 5 is somewhat extravagant in its use of steam, while also the ability to secure rapid or flash blow-off of the steam with substantially instantaneous reduction in pressure is reduced, because of the very great volume of steam to be relieved.

5

Figure 6 shows a prior art steam peeling system developed by the Applicants for the present invention, using a rotating pressure vessel 601 and various associated equipment. The vessel 601 is of generally symmetrical cylindrical form about an axis of symmetry, which extends in the plane of the paper, and the vessel 601 is rotatable about a substantially horizontal axis which, as shown in the drawing, extends perpendicular to the plane of the paper. Product is brought to the steam peeler vessel 601 by way of an in-feed container and is batched in a hopper unit 602 which supplies product through the pressure vessel 601 door opening or mouth 604 when the vessel 601 is oriented in a generally upward disposition. When the vessel 601 is sealed, rotation takes place about the substantially horizontal axis perpendicular to the plane of the paper, without rotation of the pressure vessel 601 about its axis of symmetry, and at the end of the steaming period, the pressure vessel 601 is relieved such as by valve 614 to a large volume exhaust vessel 621, for so-called "rapid flash" or expedited reduction in steam pressure within the pressure vessel 601, thereby engendering effective bursting of the peel from the surface of the product. Charging of the vessel 601 for the steaming period takes place in substantially known manner such as via valve 605 from a steam accumulator 622. Product is discharged from the pressure vessel 601 in a substantially inverted disposition thereof and is then brought by way of a product transfer auger 623 to a centrifugal separator 624, where peel is removed and discharged to waste, while the peeled product is advanced to further food processing operations as may be required.

This system has proved to be effective and economical, subject to certain disadvantageous aspects, according as understanding of the peeling process and the relevance of certain parameters of the operations carried out during peeling has become further understood.

Brief Summary of the Invention

It is an object of the invention to overcome the disadvantages of prior art peeling systems, and especially steam peeler pressure vessels, as indicated above. It is a particular objective of the invention to provide an improved steam peeler pressure vessel and also to provide an improved feed arrangement for steam peeling pressure vessels. It is a further objective of the invention to provide improved arrangements for steam discharge. It is a still further objective of the invention to provide improved arrangements in a steam peeling system for accelerating pressure relief. Yet another objective of the invention relates to effecting improvements in the manner of exhausting steam to atmosphere in a steam peeling system.

In a first aspect, the invention provides a pressure vessel for steam treatment of product to be peeled in a steam peeling system, the pressure vessel having substantially the shape of a sphere with opposed flattened side surfaces.

The pressure vessel may be defined at least in part by two opposed dish-shaped portions engaged together along rim regions of the portions to define an enclosed interior region. The two opposed dish-shaped portions are suitably welded together rim to rim to define said enclosed interior region.

In the pressure vessel according to the invention, the aspect ratio between a maximum diameter of the pressure vessel and a dimension of the pressure vessel between the opposed flattened side surfaces is preferably greater than about 1.2:1. In a specific embodiment, the aspect ratio is about 2:1.

The pressure vessel of the invention is suitably substantially symmetrical, preferably at least about an axis extending between the opposed flattened side surfaces of the pressure vessel. In a particular construction, the pressure vessel is rotatable about said axis of substantial symmetry.

According to the invention in a second aspect, there is provided a pressure vessel for steam treatment of product to be peeled in a steam peeling system, the pressure vessel being rotatable and having at least one internal lifting feature for
5 entraining and raising product relative to the axis of rotation of the pressure vessel during rotation of the pressure vessel.

The or each internal lifting feature preferably comprises a protrusion extending inwards from the region of an interior surface of a wall portion of the pressure
10 vessel, substantially in the direction of the axis of rotation of the vessel, in particular, substantially radially inwards.

The or each internal lifting feature may extend directly from the interior wall surface of the wall portion of the pressure vessel, or alternatively, it may be defined by
15 an upstanding portion of a false floor which is spaced from the interior wall surface of the wall portion of the pressure vessel. In the latter arrangement, the false floor is suitably apertured for the passage of condensate through the apertures of the false floor during use of the system, for accumulation of condensate in the region between the false floor and the interior wall surface of the wall portion of the pressure vessel, and the
20 pressure vessel may also be provided with means such as condensate discharge ports for enabling removal of condensate from the region between the false floor and the interior wall surface of the wall portion of the pressure vessel during operation of the system. In a variant, at least a portion of the false floor may be solid or non-apertured to provide a region for at least temporary retention or holding of condensate collecting or
25 accumulating during rotation of the pressure vessel.

The or each internal lifting feature may also define a closed region which is not in communication with the remainder of the interior space within the pressure vessel for the movement of gas or vapour between the closed region and the remainder of the
30 interior space within the pressure vessel.

According to a third aspect of the invention, a pressure vessel for steam treatment of product to be peeled in a steam peeling system, the pressure vessel having at least one internal region which is closed-off against ingress of steam during product treatment, said region defining a steam saver. Said internal region may be
5 defined within an enclosure, all portions of which are spaced apart from any interior wall surface of the pressure vessel.

Said at least one internal region which is closed-off against ingress of steam during product treatment may be defined in an embodiment in which the pressure vessel
10 is rotatable by an internal lifting feature for entraining and raising product relative to the axis of rotation of the pressure vessel during rotation of the pressure vessel, and said internal lifting feature may be provided in accordance with any of the variants identified under the second aspect of the invention hereinabove.

Said at least one internal region which is closed-off against ingress of steam during product treatment may also be provided on the side of a door of the pressure vessel, which side is directed towards the interior of the vessel, or by an enclosure located on a wall portion of the vessel in the vicinity of an axis of symmetry of the vessel, suitably symmetrically located with respect to the axis of symmetry of the
20 vessel. Said axis of symmetry is suitably also an axis of rotation of the pressure vessel in a rotatable embodiment of the invention. A multiplicity of said internal regions of diverse constructions may be provided within the pressure vessel of the invention. Thus lifter-defined savers may be present along with a door-mounted saver and/or a wall-mounted enclosure type saver.

25 Any or all of the three aspects of the invention as recited above may also extend to a steam peeling system comprising a pressure vessel as defined hereinabove.

30 A fourth aspect of the invention provides a rotary product batching unit comprising a plurality of compartments arranged for advancing movement within an enclosing housing, for selective successive alignment of each compartment with a

product loading location and subsequent alignment of the compartment with a product discharge location.

Each compartment of the batching unit is suitably defined between radially
5 spaced apart and radially extending blades of vanes mounted for rotation about a common axis.

The batching unit may be mounted by way of weighing means, for example a plurality of load cells, for computation of the weight of the product accommodated by
10 the batching unit.

In an alternative statement of the fourth aspect of the invention, there is provided a steam peeling system comprising a rotary batching unit for cooperation with a pressure vessel for steam treatment of product to be peeled, the rotary batching
15 unit having a plurality of compartments arranged for advancing movement within an enclosing housing, for selective successive alignment of each compartment with a product loading location and subsequent alignment of the compartment with a location for discharge of product to the pressure vessel. In this aspect also, the batching means may be equipped with a weighing feature, as described above.

20

In a fifth aspect, a steam peeling system according to the invention comprises a pressure vessel for steam treatment of product to be peeled and an expansion chamber for receiving pressurised steam discharged from the pressure vessel at the end of a steam treatment phase of a steam peeling operation, means being
25 provided for enabling release of pressurised steam from the pressure vessel into the expansion chamber, said means being located substantially at the point of entry of steam into the expansion vessel.

In a favoured embodiment, the cross-sectional flow area of the pressure releasing means increases progressively through said means from an inlet region of the
30 pressure releasing means to a discharge region of the means. Said pressure releasing means is suitably a valve.

In an alternative definition of the fifth aspect of the invention, there is provided a steam peeling system comprising a pressure vessel for steam treatment of product to be peeled, wherein pressurised steam is discharged from the pressure vessel through a port of the vessel at the end of a steam treatment phase of a steam peeling operation and the ratio between pressure vessel volume in litres and the area of said port in square inches is less than about 20:1, said port suitably being the only steam exhaust port from the pressure vessel. The pressure vessel is preferably also provided with only a single steam entry port, and the arrangement may be such that steam entry is effected through the same port as that through which steam exhaust takes place.

In a favoured embodiment, said ratio is in the range 10:1 to 20:1, more preferably about 14:1.

The invention is directed, in a sixth aspect, to a steam peeling system comprising a pressure vessel for steam treatment of product to be peeled and an expansion chamber for receiving pressurised steam discharged from the pressure vessel at the end of a steam treatment phase of a steam peeling operation, means being provided for release of steam and/or vapour from the expansion chamber to atmosphere, said means comprising an arrangement for substantially minimising release of entrained solid matter and/or odours in steam and/or vapour leaving the expansion chamber.

In a particular construction of steam peeling system in this aspect of the invention, a baffle is located within the expansion chamber and a solids trap is located substantially at the exit location from a stack communicating between the interior of the expansion chamber and atmosphere. Alternatively, a solids trap may be located in the interior of the expansion chamber.

According to a seventh aspect, a steam peeling system in accordance with the invention comprises a control system for regulating movements of a pressure vessel for steam treatment of product to be peeled between loading and discharge

dispositions of the pressure vessel through a succession of treatment stages, unproductive displacement of the pressure vessel being substantially minimised during said movements.

5 The control system preferably provides for discharge of product from the pressure vessel while the vessel is in motion during a treatment/process cycle. In a favoured embodiment, provision is made for opening and/or closing of a door portion of the pressure vessel while the vessel is in motion during a treatment/process cycle.

10 The pressure vessel is suitably rotatable and the control system may provide for reversal of the direction of rotation during a treatment/process cycle. The direction of rotation during dump or discharge of product from the pressure vessel is preferably opposite to the direction of rotation of the pressure vessel at the start of the treatment/process cycle.

15 The control system may also provide for variation of speed of movement of the pressure vessel during a treatment cycle, as well as for discharge of product from the pressure vessel while the vessel is in motion during a treatment/process cycle.

20 The invention additionally extends to a pressure vessel for steam treatment of product in a steam peeling system, substantially as described herein with reference to and as shown in any one or more of Figures 7 to 19 of the accompanying drawings, as well as to a rotary batching unit, substantially as described herein with reference to and as shown in any one or more of Figures 7 to 11 of the accompanying drawings, and a
25 steam peeling system, substantially as described herein with reference to and as shown in any one or more of Figures 7 to 24 of the accompanying drawings.

Brief Description of the Drawings

30 The invention will now be described with reference to the accompanying drawings, of which Figures 1 to 6 illustrate selected significant features of a number of prior art arrangements relating to steam peeling, Figures 7 to 16 illustrate the peeler

vessel according to the invention in a first embodiment, along with associated equipment. Figures 17 to 20 illustrate variants of the peeler vessel for a system according to the invention. Figures 21 to 24 relate to arrangements for trapping or entraining solids and reducing odour in exhaust emissions as well as accelerating
5 pressure reduction during steam discharge from the pressure vessel.

In detail:

Figure 1 shows a first prior art arrangement of rotating pressure vessel for
10 steam peeling food products,

Figure 2 shows a second prior art arrangement of rotatable pressure vessel for steam peeling food products,

Figure 3 shows a third prior art arrangement of rotatable pressure vessel
15 for steam peeling food products,

Figure 4 shows a first prior art arrangement for steam peeling food product in which a static pressure vessel is used,
20

Figure 5 shows a second prior art arrangement for steam peeling food product in which a static pressure vessel is used,

Figure 6 shows a further prior art steam peeling system in which a
25 rotatable pressure vessel is used,

Figure 7 is a side view of the novel rotatable steam peeling vessel and associated features provided by the invention,

Figure 8 is an end view from the righthand side of the arrangement of
30 Figure 7,

Figure 9 is a top or plan view of the arrangement according to Figures 7 and 8,

5 Figure 10 is a diagrammatic side view of a steam peeling pressure vessel and associated feed hopper according to the invention, operating in a first stage of a feed or loading operation,

10 Figure 11 corresponds to Figure 10, showing a feed or loading operation in a second stage,

Figure 12 is a central sectional side view of the steam peeling pressure vessel provided by the present invention, showing internal features of the vessel,

15 Figure 13 is a sectional view of the vessel of Figure 12, on the plane A-A of Figure 12,

Figure 14 is a top or plan view of the pressure vessel of Figures 12 and 13,

20 Figure 15 is an end view of a rotatable steam peeling pressure vessel according to the invention, showing rotary drive and steam feed and exhaust arrangements,

25 Figure 16 is a rotational programme diagram for one complete steam peeling cycle for a steam peeling pressure vessel in accordance with the invention,

Figure 17 shows details of an in-vessel condensate removal feature of the steam peeler vessel of the invention, in diagrammatic side sectional view,

30 Figure 18 shows a diagrammatic sectional view of the peeler vessel of Figure 17, on the plane B-B of Figure 17, but with omission of certain features,

Figure 19 shows details of a variant of the in-vessel condensate removal feature of Figure 17, again in diagrammatic side section or view,

5 Figure 20 shows a known construction of steam peeler vessel fitted with condensate separation features and also incorporating product lifting or mixing features in accordance with the invention, in diagrammatic side sectional view,

Figure 21 is a diagrammatic top view of the modified peeler vessel of
10 Figure 20, on the plane C-C of Figure 20, again with omission of selected features not essential to understanding the invention in this variant,

Figure 22 shows a first exhaust arrangement in a system in accordance with the invention, as well as features for encouraging accelerated pressure drop in an
15 expansion chamber, and

Figure 23 shows a second arrangement for solids entrainment in the exhaust features of a system in accordance with the invention.

20 Detailed Description of the Drawings

Figures 1 to 6 inclusive relate to prior art peeling systems and have already been discussed.

25 Referring now to Figures 7, 8 and 9, there is shown a steam peeling system according to the present invention, incorporating a steam peeling pressure vessel 1 in accordance with the invention and including also other features according to the invention. As shown in the side view of Figure 7, the steam peeling vessel 1 is mounted for rotation about an axis 7 which extend substantially horizontally and
30 perpendicular to the plane of the paper. The pressure vessel 1 is supported for rotation on a structure also providing operator access to the system, whenever required. Infeed to the pressure vessel 1 is provided by a conveyor belt 26 to a rotary

batching unit 2, by which product is transferred from the infeed belt 26 to the pressure vessel 1 in measured quantities, as subsequently described. The representation of the human Figure 27 in Figures 7 and 8 is intended to indicate the scale of the system in an exemplary embodiment.

5

Referring now in particular to Figure 8, the relative dispositions of the batching unit 2 and the pressure vessel 1 are again shown, together with the relationship between the pressure vessel 1 and an expansion chamber or vessel 21 which is located to the rear of and below the pressure vessel 1 in terms of Figure 7.

10 As indicated in Figures 8 and 9, a large diameter stack 28 extends from the expansion chamber to a discharge location (not shown in these drawings) for waste or exhaust steam, the arrangement in this regard to be described below. The expansion chamber 21 is provided with special fast condensing facilities, again as subsequently described. The compact arrangement of the various units of the system may be noted, the
15 assembled system defining an especially cohesive package occupying a reduced spatial volume as compared with prior art arrangements.

Referring finally to the top view of Figure 9, the relative dispositions of these various features will be again apparent, and in particular, as also shown in
20 Figure 8, the locations of the bearings 29, 31 for the rotary pressure vessel 1 and also the disposition of the steam line 14 between vessel 1 and expansion chamber 21 are particularly apparent. Also shown in Figures 8 and 9, and not illustrated in subsequent drawings, are drive motor and drive gear arrangements 32 and 33 respectively for vessel 1 and batching unit 2 respectively.

25

As compared with prior art peelers, the pressure vessel 1 of the present invention is particularly suited to being embodied in units of dimensions suited to the treatment of lesser volumes of product than in the prior art. However, despite a reduced pressure vessel capacity system, throughput is not reduced, because of an
30 accelerated cycle time and particularly efficient use of all stages of the cycle, as will be subsequently explained.

Figures 10 and 11 show, in their loading dispositions, the rotary pressure vessel 1 and the cooperating rotary batching unit 2, which takes the form of a rotary batch hopper. As shown in Figure 10, the pressure vessel 1 is rotated about its axis of rotation 7 into a disposition in which the charging and discharging opening or mouth 4 is directed upwardly at an angle. The door 6, which closes from the interior, is at this time also in an open disposition. In this orientation, the pressure vessel 1 is aligned with ducting features 34 facilitating product movement from the rotary batch hopper 2 into the pressure vessel 1.

10

The rotary batch hopper 2 consists of a substantially cylindrical drum 35, which is stationary, and has inlet 36 and outlet 37 ports. The inlet port 36 is located underneath the delivery end of the product conveyor 4, while the outlet port 37 is aligned with the ducting features 34 through which product 3 may move from the rotary batch hopper 2 into the pressure vessel 1. Within the rotary batch hopper 2, there are provided a number, preferably six, of vanes or blades 38, together defining a structure somewhat similar to a paddle wheel. The vanes or blades 38 rotate as a single integral unit within the static cylindrical shell 35 of the rotary batch hopper 2 and thereby define a series of moving compartments 39. Product 3 falling from the conveyor 26 enters into the particular compartment 39 which is currently aligned with and stationary at or moving past the inlet port 36 of the hopper 2. Indexing may be used in operation of the batcher 2 for loading alignment of compartments 39 by intermittent advance of the blades or vanes 38. As the blade 38 defining the trailing edge of the space 39 in question moves away from the inlet port 36, the particular segment 39 of the rotary batch hopper 2 which is now charged with product 3 to a substantially predetermined extent is closed off against entry of further product 3 and continued rotation of the blades 38 brings this compartment 39 into traversing alignment with the ducting 34 giving admission to the peeling vessel 1, where product 3 falls from the compartment 39 into the pressure vessel 1, as shown in Figure 11.

30

The delivery from the conveyor 26 and the advancing rotary movement of the vanes 38 of the batch hopper 2 may be coordinated and linked for intermittent

advance in a manner suitable to load substantially measured quantities of product 3 into the pressure vessel 1. In a preferred arrangement, the batch hopper 2 is used to load four segments 39 of product 3 into the pressure vessel 1, for a high capacity load. A low capacity peel is also possible, in which the contents of the batch hopper 2 to be transferred to the peeler 1 are contained in just two or three segments 39 of the hopper 2. It will be apparent that still further arrangements may be provided, in which different numbers of segments 39 are used for product 3 loading, or hoppers 2 with different numbers of blades 38 are provided, as for example, the five-bladed variant illustrated schematically in Figure 7.

10

The rotary batching unit 2 according to the present invention as described and shown with respect to Figures 10 and 11 also provides for product weighing. Thus the batcher 2 is also used to weigh product 3 being fed to the pressure vessel 1. For this purpose, the batcher is suitably mounted on three load cells and the weight of product accommodated within the unit may be evaluated continuously. The weight of product discharged and/or received may then be completed by suitable coordination between the weighing operation and vane displacement. In this way, the weight of product in any compartment of the batcher may be determined.

20

The unit 2 has multiple advantages, in that it is particularly simple, having just two bearings and being drivable by a relatively small motor 33 (Figure 9). There is a gentle fill from the infeed elevator or conveyor 26 to the batching unit 2, the drop height being low, in a preferred embodiment less than 600mm, although greater drops may be employed without product 3 being damaged. The manner of movement of product 3 within the unit 2 from when it is loaded into the batcher 2 to when it is discharged to the peeler 1 also substantially precludes product 3 damage at this stage also. There is thus likewise a gentle fill from the batching unit 2 itself into the pressure vessel 1. The batcher 2 may be described as operating as a kind of "lowerator" for the product 3. This gentle fill or "lowerating" effect may be achieved at both high and low capacity batch loads. The method of loading reduces possible product 3 damage during transfer of product 3 from infeed conveyor 26 to the pressure vessel 1.

30

The unit 2 requires low maintenance and provides high reliability, in that there are no belts or rollers, and no sliding door, such as exists in known batching units. Weighing may be effected by load cells.

5

The unit 2 is particularly easy to fill into from the infeed conveyor 26, even when a wide unit 2 and a wide conveyor 26 are used. No cut-outs are required in the hopper 2. The construction is such that product 3 cannot bridge, in that there is no taper in the directions of either loading or discharge. The unit 2 facilitates the handling of small batches, by virtue of the segmented 39 construction. The unit 2 may be readily manufactured and is of low cost, even when manufactured in stainless steel. It further enables the overall height of the steam peeling system to be significantly reduced, while allowing venting of the cladding for the steam region. The use of a rotary batching unit 2 of this type in steam peeling, together with associated weighing and feeding, represents one novel aspect of the present invention, and one providing a uniquely attractive visual and technological ambience to the system of the invention. Figures 10 and 11 also indicate in part certain structural supporting features 41 relating to the mounting of the pressure vessel 1.

Referring now to Figures 12, 13 and 14, these show structural and internal details of the pressure vessel 1. A simple shell structure of the general shape of a solid doughnut, namely one without a central aperture, is used. In other words, in this embodiment, the structure 1 resembles a sphere with squashed-in sides, 42, 43, but a wide diversity of other shapes and constructions may be applied. The structure 1 is rotatable about an axis 7 extending between the two somewhat flattened sides. The simplicity of the structure is particularly advantageous for construction as a shell. The pressure vessel 1 may be assembled from two dished portions, for example, ellipsoidal dished ends, welded together along their rims.

It is important to emphasise that the reference to "a sphere" in describing the shape of the pressure vessel 1 of the invention is for the purposes of such description only and the present inventive unit 1 in no way equates to a wholly spherical pressure

vessel as known in the prior art. Thus in referring to the unit 1 of the invention as being in the shape of a solid doughnut, what is in question is a so called jam doughnut, rather than a doughnut with a central aperture passing through it. As noted, the unit 1 may be formed from two dished shells, fixed together such as by welding along their rims. An
5 ellipsoidal cross section may suitably be used for each shell, but this shape is not an essential aspect of the unit 1 according to the invention. The vessel 1 of the invention is to be distinguished from any fully spherical unit of the prior art by its aspect ratio, namely the ratio of the maximum diameter of the pressure vessel 1 to its width, this latter being defined as its wall to wall dimension substantially along its axis of rotation 7, i.e.
10 between walls 42 and 43. For a sphere, as in the known pressure vessel, the aspect ratio is 1:1, whereas in the unit 1 of the invention, the aspect ratio is in the range from 1.2:1 upwards, e.g., in a typical construction of the order of about 2:1. Thus the overall shape of the unit 1 is somewhat similar to that of a low aspect tyre as applied in modern high performance motor vehicles.

15

As shown in the drawings, bearing mountings 44, 45 are provided on the flat side faces 42, 43 of the pressure vessel 1, and one 44 of these bearing mountings 44, 45 is provided with a single opening or port 46 for steam discharge, as subsequently described and discussed. On the top of the unit 1, in the orientation
20 shown in the drawings, there is provided the peeler vessel product 3 inlet port or mouth 4, which is closed off by an inwardly pivotable door 6. The door 6 may be provided on its underside with a surface portion 47 which defines, in the closed condition of the door 6, a substantially smooth continuation of the internal surface 48 of the pressure vessel 1 throughout the door 6 region. An arrangement of this kind
25 serves to prevent product 3 from becoming trapped in any constricted regions of the interior of the pressure vessel 1 during pressure vessel 1 rotation, but does not represent an essential feature of the invention.

The smoothing 47 of the internal profile 48 by a door infill of this nature
30 may also be advantageous to avoid possible engagement of product 3 by the ducting 49 in the door 6 region during rotation at higher speeds with any potential product 3 throwing situation being thereby avoided. However, within the normal speed range

applicable to the system of the invention, such a situation does not in the normal way arise and in-filling of the door 6 region represents an optional feature only.

The internal shape of the vessel 1 is also adapted to assist in lifting product
5 3 held within the vessel 1 during rotation, to ensure constant product 3 movement during vessel 1 rotation. Such lifting/mixing action enables more uniform peeling to be achieved, due to more uniform application of steam to the product 3. Lifting features 51a, 51b and 51c within the vessel 1 are shown in the drawing, in the form of inward protrusions from vessel internal surface 48. Lifting features 51a, 51b, 51c of
10 this kind may also be defined or referred to as paddle lifters, and a multiplicity of such features may be used, for example three in an exemplary embodiment as shown in Figure 12. This feature of the invention is of particular significance and advantage and is further described below.

15 The pressure vessel 1 according to the invention also incorporates steam savers. Steam savers consist of fillers within the vessel 1 which cut down the amount of free space inside it, thus saving steam and optionally also advancing the mixing action. In a pressure vessel 1 of a particular nominal capacity, a volume significantly less than the nominal capacity would suffice to accommodate product 3 during steam
20 peeling. While a larger volume is needed to ensure mixing, steam savers are used to fine-tune the volume requirement and reduce the unnecessary or wasted space to the minimum required to enable mixing. One such steam saver 51a, which also defines a lifter, is shown adjacent to the door 6 and to the right of the door 6 in Figure 12. This provides a projecting enclosed region 51a extending into the internal space 16 of the
25 pressure vessel 1 from the wall 48 thereof. The steam saver 51a thus represents or defines a sealed-off region of the interior of the pressure vessel 1, into which steam cannot penetrate, and neither, of course, can product 3. A further steam saver 52 is provided on the rear face of the door 6 itself, in that the region between the outer panel of the door 6 and the inner curved portion or panel 47 which matches the
30 internal surface 48 of the pressure vessel 1 is also sealed against steam entry. In addition, the further mixing bars or lifting paddles 51b and 51c may also constitute small steam savers, either in the structural form as shown in Figure 12 or alternatively

in the form of closed-off or sealed cylinders mounted on the inner wall 48 of the vessel 1, while a still further steam saver 53 is provided by an additional encroachment or closed-off domed region overlying the non-steam passage-provided bearing mounting 45 of the pressure vessel 1, namely that on the righthand side as it appears in Figures 13 and 14. At the lefthand bearing mounting 44 as shown in Figure 13, i.e. that bearing mounting which is provided with the steam entry and exit passage 46, a perforated head or baffle 54 located in the interior 16 of the vessel 1 and covering over the entry to the steam port 46 from the vessel 1 interior 16 allows entry and exit of steam, but not the passage of product 3. Thus product 3 to be peeled, which is held within the vessel 1, cannot reach the steam feed and discharge duct 14. Steam savers are seen as a particularly advantageous feature of the present invention, in that not only do they reduce the cost of steam supply but they also enhance exhaust time, because there is less steam to be exhausted. In a particular construction, two small lifters 51 serving also as steam savers and one large filler 52 or 53 may be provided, the large filler being selected from one or other of the options 52 or 53 shown in the drawings, although provision of multiple lifters 51 also doubling as steam savers is not precluded. In a further variant, up to six lifters 51 may find application, one or more also optionally defined by steam saver features of the structure.

20

It may be emphasised that any region of the vessel 1 which is not used for the treatment of product 3 may be employed as a steam saver. Thus in addition to the various examples of steam savers shown in the previous drawings, a further steam saver may be provided across the centre of the vessel 1, being defined by a closed drum extending transversely across the vessel 1 and in coaxial surrounding alignment with the axis of rotation 7 of the vessel 1. In a still further variant, a closed-off, substantially spherical region defining a steam saver may be defined in this part of the pressure vessel. The deployment of unused regions of the vessel 1 for steam savers is additional to savers defined by lifters 51, which, by contrast, are deployed within active or operative regions of the vessel 1.

30

Thus, each of these steam savers may define a lifting member or bar 51, although, as already mentioned, lifters 51 may also be defined independently of steam savers. Lifters 51 may be applied not only to pressure vessels 1 of the present novel configuration but also in peeling vessels of known configuration. Likewise, steam
5 savers may be applied in peeling vessels of known construction, either in combination with lifters and, at least in part, defining lifters, or entirely independently of any provision of lifters.

Experimental investigations have shown that in the absence of lifters 51,
10 there is a tendency for product 3 to remain static at the base of the vessel 1 during rotation, the aggregate of product 3 within the vessel 1 behaving somewhat similarly to liquid or sand in such circumstances. In a particular arrangement, illustrated in Figure 12, each lifter 51 is defined by a generally L-shaped, right-angled plate portion, shaped on the outer edges of each angle member to fit the curved internal profile 48 of the
15 steamer vessel 1 and placed in position with the 90° angle directed inwards, the angle plate edges being welded to vessel wall 48. Thus steam saving regions are thereby also defined in the interior of each lifter 51. As shown in the drawings of the present application, three sizes of lifter 51a, 51b and 51c may be used, and they may be spaced apart at substantially 120° intervals around the internal periphery 48 of the vessel 1,
20 with the largest lifter 51a being closest to the filling opening 4 and located on that side of the filling opening 4 where the duct portion 49 communicating between the vessel 1 mouth 4 and the interior 16 of the vessel 1 has the shortest axial dimension. Moving away from this shorter axial dimension side of the entry region 4, the lifters 51a, 51b, 51c are then in succession respectively large, medium and small in the peripheral or
25 circumferential direction of the vessel, i.e. clockwise in Figure 12.

The provision of steam savers 51, 52, 53 according to the invention enables precise computation or calculation of the saving in steam to be achieved by use of a system according to the invention, as compared with prior art steam peeling
30 arrangements. Minimisation of the quantity of steam required by the system during product treatment also assists in speeding up exhaust, in that there is a lesser amount of steam to be discharged during the exhaust phase. Steam savers 51, 52, 53 may be

dimensioned and selected such that the effective operating volume of a pressure vessel 1 in a particular installation may be varied, within a substantially standard external shell. Furthermore, as described above, steam savers 51, 52, 53 may be provided within the pressure vessel 1 to be of dimensions and configurations such as
5 will assist in mixing and agitation of product 3 to be treated.

An optional feature of the invention is also shown in Figure 12, in the form of a door weight counterbalance 55 provided to improve the speed capability of the vessel 1 in rotation, namely the ability of the pressure vessel 1 to rotate at a faster rate.
10 Thus the unique and novel pressure vessel 1 shape provided by the invention combined with its other features establish a potential for high speed operation, with the steaming action within the vessel 1 being further enhanced by the provision of the mixing lifters or paddles 51a, 51b and 51c according to the invention. In a practical installation, counterweight 55, showed spaced from the vessel 1 outer wall, is actually
15 mounted on the vessel 1.

Moving now to Figure 15, the pressure vessel 1 rotating mounting and steam discharge arrangements are shown. On the righthand side of the pressure vessel 1, drive 33 is effected at the righthand bearing mounting 45 and bearing 31
20 (Figures 8 and 9) as shown in the drawing. On the lefthand side of the drawing, steam entry and exit is effected through the lefthand bearing mounting 44 and bearing 29 (Figures 8 and 9). Communication between the interior 16 of the pressure vessel 1 and the steam charging and discharge line 14 is effected through a rotary gland 56 with suitable packing. Thus steam admission and steam discharge takes place
25 through a single steam port. There is only one port in the system, and this port serves alternately as an inlet port and an exhaust port. Steam is fed into the pressure vessel 1 through a charging line, not shown in the drawing, by way of a suitable valve arrangement 5. Beyond the charging connection 5, the steam passage 14 from the pressure vessel 1 terminates at an expansion valve 57, which is mounted directly at
30 and suitably on top of the expansion chamber 21 and defines a steam pressure release means of the system. The valve 57 geometry provides for an inlet diameter of substantially 10 inches and an outlet diameter of 12 inches, so that expansion of steam

being conducted through valve 57 takes place in part through and within the actual body of valve 57. The increase in area from valve inlet to valve outlet is thus of the order of 40%. The arrangement provides a spatial saving and may also be associated with a reduction in noise and flow turbulence at the point of entry into the expansion chamber 21, as well as a reduction in the number of components in the system and less back pressure. Valve 57 is suitably motor driven 58.

The 10 inch inlet diameter to the expansion valve 57 together with the provision of a comparable diameter and exhaust flow area at the single exhaust port 46 of vessel 1 represents a very substantial increase in pressure vessel 1 exhaust port 46 diameter and area as compared with the maximum values currently in use, at least in single port steam peeler pressure vessel arrangements, where exhaust port diameters are typically in the range of 7 to 8 inches. As already noted, exhaust port 46 defines a single port for the pressure vessel and also serves as the steam admission or inlet port. Thus there is, in the system of the invention as embodied in the present drawing, a single entry port and a single exit port. As a result of this increase in pressure vessel 1 exhaust port 46 size, together with the use of an expansion valve 57 mounted at and on the expansion or blowdown chamber 21, a significantly reduced ratio of peeling pressure vessel 1 volume to exhaust port 46 area applies in the system of the invention. Specifically, the ratio between vessel 1 volume in litres and port 46 area in square inches is typically as follows:

		Pressure vessel 1 volume (litres)	Port 46 area (sq. inches)	Ratio (vol: area)
25	PRIOR ART	1400	50.2	27.9:1
	INVENTION	1000	78.55	12.7:1
		1100	78.55	14:1
		1200	78.55	15.2:1

30 The ratio may also be expressed between vessel 1 volume and port 46 diameter, resulting in the following figures:

	Pressure vessel 1 volume	Port 46 diameter	Ratio
	(litres)	(inches)	(vol:diameter)
5 PRIOR ART	1400	8	175:1
INVENTION	1100	10	110:1

The preferred ratio of vessel 1 volume to discharge line 14 diameter provided
 by the invention facilitates optimisation of the bearing 29 (Figures 8 and 9) surrounding
 10 the discharge line 14 between the vessel 1 and the steam gland 56 and steam valve 5
 region. This bearing 29 is exposed to particularly difficult operating conditions and the
 system parameters provided by the invention facilitate substantially optimised bearing
 29 selection. It will be appreciated that the enhanced steam line 14 diameter and area
 provided by the invention prevails throughout line 14 from exhaust port 46 through to
 15 the comparably sized or dimensioned inlet to expansion valve 57.

This arrangement according to the invention provides several
 advantageous improvements. The bore of the passage 14 leading from the pressure
 vessel 1 to the expansion chamber 21 is larger than in known constructions. An
 20 increase in steam duct or passage 14 diameter to 10 inches or 250mm using a single
 outlet or port 46 from pressure vessel 1 such as is provided in a preferred embodiment
 of the pressure vessel 1 according to the present invention represents a very
 substantial increase in flow area, as compared with a prior art single port diameter of
 200mm. The capacity of the exhaust valve 57 is likewise also increased compared
 25 with prior art arrangements, as already noted above, as also is the size of the
 expansion chamber 21. These improvements result in extremely rapid discharge of
 steam from the pressure vessel 1 to provide expedited clearance of pressurised steam
 from the pressure vessel 1. Applicants' prior art system of Figure 6 provides a
 clearance time of between 3 and 7 seconds, this being itself significantly better than
 30 many other known systems, in which discharge can take as long as 12 seconds, so that
 the further gain achieved by the present invention can be seen to be particularly
 significant.

In the arrangement of the invention, the expansion valve 57 is exposed to pressurised steam during peeling and opens directly into the expansion vessel 21 at the appropriate time. The use of as large an expansion chamber 21 as possible means
5 that discharge directly to atmosphere is to a significant degree simulated.

Environmental regulations reasons generally prohibit or exclude the possibility of direct discharge to atmosphere, hence the necessity to interpose an expansion chamber 21, but the desirability of achieving the maximum possible rate of pressure drop into the expansion chamber 21.

10

As shown schematically in Figure 15, the expansion valve 57 is an elbow valve with the internal diameter of the flow passage increasing from 10 inches on the input side to 12 inches on the output or discharge side of the valve 57 at the expansion or blowdown chamber 21. Proceeding along the steam line 14 from the 10 inch input
15 side of the valve in the direction of the pressure vessel 1, there are provided in sequence, from the elbow valve 57 end, the steam valve 5, the rotating steam gland 56 with balancing features (not shown), and a pipe section 14 of 10 inches diameter passing through the main bearing 29 (Figures 8 and 9), this large diameter pipe section 14 providing for both steam-in and exhaust. Where the steam input or exhaust line 14
20 enters the pressure vessel 1, the terminal region is covered by the baffle 54 which is a meshed grid having apertures or holes of relatively large size, matched to product size, to stop product 3 exiting into the expansion chamber 21 during the expansion phase. Steam is thus blown in through this perforated baffle 54 and pressurised steam exhausts through it during the exhaust phase. While the baffle 54 prevents exit of whole product
25 3, the very rapid discharge of steam results in considerable carry-over of fragments of peel and other solid matter, which is not inhibited by the relatively large perforations of the baffle 54, but there is no accumulation of such matter in the expansion vessel 21, as the vessel 21 is flushed out at frequent intervals, and any solid matter carried into it tends to be entrained/liquidised and removed through a drain or solids separation facility
30 provided in chamber 21.

The combination of features provided by the invention result in substantially instantaneous reduction in pressure in the steam peeler vessel 1 when exhaust takes place. By substantially instantaneous is meant a pressure drop taking place in a time period which is typically less than 1 second. It is not necessary to programme any exhaust time as such, as the exhaust phase is delimited by the very rapid release of pressure from the peeler vessel 1 and by the valve 57 opening time, which is also very short. Thus by mounting the exhaust valve 57 substantially directly on or at the decompression or expansion vessel 21, the invention provides for substantial maximisation of the possible pressure drop. The exhaust vessel 21 and expansion valve 57 are accordingly effectively combined, for optimisation of the pressure drop. There is no separate duct communicating between expansion valve 57 and chamber 21. The exceedingly rapid blowdown achieved by the invention may be further augmented or enhanced by vacuum effect or like arrangements within the chamber 21, such as water spray, subsequently described. There is therefore effectively instant exhaust via the exhaust valve 57 and the very short steam exhaust path or line 14 from the peeling vessel 1 to the expansion vessel or chamber 21.

Figure 16 shows a rotational programme for a pressure vessel according to the invention for one complete cycle. Clockwise and anticlockwise are referred to the unit 1 in the orientation of the miniature representation of Figure 12 in the top left hand corner of Figure 16. Initial rotation is clockwise from the disposition of Figure 12 so as to ensure that any product 3 in the vicinity of the door 6 falls away from the door port 4 and does not interfere or block the closing action of the door 6. The operation commences from the upwardly oriented loading position of vessel 1. Following loading of product 3 with closure of door 6, rotation commences to the right during this period of the rotation, i.e. clockwise as shown in Figure 16, at an initial speed of for example about 10 rpm, accelerating to typically about 16 to 18 rpm. This phase of the rotational programme is designated by reference 59. This initial rotation as shown is carried through approximately 170° , but the precise angular extent of this phase of the rotation is dependent on steam time. Rotation is then reversed, the pressure vessel 1 returning anticlockwise initially for example at a

rotational speed of the order of 16 rpm and then slowing and accelerating again, before finally slowing to a rotational speed of suitably approximately 6 rpm as the door 6 region moves into towards a downwardly oriented disposition. This phase of the rotational programme is designated by reference 61. This reversal of rotation is an especially significant feature of the rotational programme according to the invention. In particular, the initial rotation from the start position is in the opposite direction to the direction of rotation during the final dump or discharge operation. The reversal of the direction of rotation is effected during the process, i.e. during the steam/exhaust phase. Prior art peelers involving rotation of a pressure vessel rotate in the dump direction from the start of the treatment process and there is no reversal of direction. While the vessel 1 is directed upwardly during this reverse or return phase of rotation, the steam pressure within the pressure vessel 1 is relieved and the door 6 opened, door opening taking place during vessel rotation, so that as the rotational cycle proceeds into the orientation of the pressure vessel 1 in which the door 6 region and the discharge and loading port 4 are downwardly directed, i.e. region 62 of the second phase of the rotational programme (reference 61) in Figure 16, the door 6 is then open so that product 3 can discharge in an unobstructed manner through the port 4 onto downstream handling equipment. Speed is reduced to of the order of 6 rpm during this discharge period of the rotational programme, while the door 6 is open and directed downwardly. As the vessel reaches the 135° position as shown in Figure 16, rotation is again accelerated to about 16 rpm to bring the now open port 4 back to the loading position, where rotation stops at reference 63 and a further batch of product 3 is charged to the pressure vessel 1 and the entire cycle commences once again. The speeds achieved during rotation in the system of the present invention are in the range of 6-20 rpm, as compared with a range of 6-10 rpm in the prior art.

The speed of rotation is relevant to the quality of the mixing. In known peeling vessels of drum-shaped configuration, the peripheral speed of product closer to the axis of rotation is considerably lower than that of product at the maximum radius or spacing from the axis of rotation. By contrast, in the unit 1 of the invention, substantially uniform peeling performance is achieved at all locations throughout the

pressure vessel 1 because of product 3 being disposed at substantially constant radius during the treatment process and also because there is effective mixing action of product 3 during rotation so as to ensure that each product item 3 is exposed to substantially uniform conditions, both in terms of exposure to steam and travel, in
5 aggregate over the duration of an operating cycle.

The rotational programme provided by the present invention is particularly efficient, in that there is a minimum of wasted time. By reversing rotation following an initial steaming period and relieving the steam pressure and opening the door 6
10 during the reverse rotation, the product 3 is ready for rapid unloading or discharge within substantially an absolute minimum of time from the start of the steam cycle. Relieving pressure and opening the door 6 during that segment of the reverse rotation 61 during which the door 6 and the port region 4 are directed upwards also means that an inwardly-opening door 6 may be successfully actuated and opened without
15 encountering or being hindered by product 3 within the pressure vessel 1. In prior art arrangements, where unidirectional rotation is in question, the product may require to remain in the pressure vessel for a rotation period which is required solely for port orientation purposes, but is not necessary from the point of view of peeling treatment. Travel between completion of the unloading and positioning of the inlet port 4 for
20 receipt of the next product 3 load is also substantially minimised. Thus in the system of the invention, every phase of the rotational programme is constructively used for some defined and necessary activity, and unnecessary or wasteful displacements and/or operations are substantially eliminated or minimised. This is especially the case in respect of the door opening and closing operations, which are effected during
25 rotation, thereby saving time, since these operations are typically effected when the vessel is static in known constructions. The enhanced rotational programme of the invention accordingly provides effectively substantially non-stop rotation, including a reversal of direction, but without this reversal entailing any significant standstill period other than a momentary stop condition for reversal of drive, except during the
30 filling phase. Rotation does not stop for discharge or unloading of the pressure vessel 1, which takes place however during a reduced-speed portion of vessel 1 rotation. The rotational programme is established by suitable control systems, which

may be embodied in software, and to which the scope of the invention also extends. Reversal may also be effected at any time, while the direction of initial rotation after filling, as indicated above, allows greater loads to be accommodated.

5 These features of the invention, in particular reversal of rotation, are particularly facilitated by the relatively small size and low rotational inertia of the pressure vessel 1 according to the invention, especially as compared with prior art units. The unit 1 of the invention is also distinguished by being particularly well-balanced. The unit 1 of the invention is thus distinguished from the prior art or
10 known peelers by providing for rotation in both directions as compared with the unidirectional rotation of conventional arrangements. Along with this reversal of rotation, the control system further provides for dead time to be minimised as compared with the steam time.

15 Figures 17 and 18 show a variant of the invention providing for separation and/or removal of condensate within a pressure vessel 1 in accordance with the invention. As shown in these drawings, a perforated or apertured condensate floor or liner 64 is provided around the periphery 48 of the vessel 1, extending substantially from the vicinity of one side 65 of the entry point 4 in the circumferential or peripheral
20 direction over approximately three quarters of the circumference 48, to terminate in the clockwise direction as shown in Figure 17 slightly short of the opposite side 66 of the entry duct 49 or port 4. Alternatively, the liner 64 may extend right up the side 66 of the entry duct 49. The floor 64 commences at the short axial extent side 65 of mouth 4 ducting 49 and terminates short of the other side 66 of ducting or nozzle 49 which is of
25 greater axial extent. As shown in the drawings, two condensate removal ports 67 are provided so that condensate may be extracted or removed from the vessel 1 while the vessel 1 is in motion. This aspect of the arrangement is however, optional, and condensate separated from product 3 during rotation of the pressure vessel 1 may merely remain within the vessel 1 underneath the perforated liner 64, either in the lower portion
30 of the vessel 1 under the action of gravity, or alternatively by being engaged against the inner side 48 of the outer wall of the vessel 1 by centrifugal force. This perforated liner or apertured condensate floor feature 64 of the invention is particularly relevant to

small product, such as for example, small carrots. The provision of this condensate separation feature 64 within the pressure vessel 1 avoids product 3 lying in condensate at any time during the peeling phase and in particular during the rotational action.

5 As shown in Figure 17 in particular, in this variant of the invention, the lifters 51a, 51b and 51c are incorporated in the false bottom or condensate liner 64. The lifters 51a, 51b and 51c are defined by a series of internally directed indents or protrusions in the perforated floor 64. As compared with previous embodiments, the lifters 51a, 51b and 51c in this variation do not take the form of steam savers. As
10 previously indicated, the lifting or agitating or mixing effect achieved by the lifter features 51a, 51b and 51c according to the invention is independent of the steam saving aspect of the invention, although it may in certain embodiments be provided by combining lifting and steam saving. In the arrangement of Figures 17 and 18, lifting is effected by the radially inward projections 51a, 51b and 51c of the perforated
15 condensate floor 64 and these are provided entirely separately from any possible steam saving feature.

The provision of a false floor 64 or other arrangement for separation of condensate is said to be justified in order to avoid product 3 undergoing peeling
20 treatment from sitting in condensate when condensate is formed, with the establishment of a barrier by this condensate against fast heat transfer between steam and product 3.

The condensate barrier is said to lead to longer steam times being necessary and thus lower yields by virtue of higher peel and flesh loss. A second justification for
25 condensate separation and/or removal is said to be that if condensate has not been removed, a proportion of it will flash back to steam, at the exhaust stage, thus increasing the exhaust or steam evacuation time. However, any possible condensate barrier problem is less significant when the product 3 is of relatively large dimensions, such as a large potato, because the amount of condensate formed on large product 3 is relatively
30 small and is insufficient to cover even part of the surface region of the product 3. Secondly, in the system of the invention where the rotation is relatively fast, product 3 is constantly moving with a high degree of mixing and product distribution, so that no

individual product 3 has the opportunity to remain in contact with condensate for more than a brief period of time. Thus the necessity for separation of product 3 from condensate is by and large limited to very small products, such as baby carrots, in which circumstances the provision of the false bottom arrangement 64 described above
5 becomes appropriate. Even in such circumstances, there is no effective time saving, in a system in accordance with the invention, due to less condensate being flashed off to exhaust, because of the significantly accelerated and very brief exhaust time achieved in the novel peeling unit 1 according to the invention.

10 Figure 19 shows a further variant of the invention providing for separation and/or removal of condensate within a pressure vessel 1 in accordance with the invention. As shown in this drawing, the condensate floor or liner 64 is again provided around the periphery 48 of the vessel 1. As compared with Figure 17 however, in this variant, end regions 64a, 64b of the floor 64 are imperforate or non-apertured, i.e. solid,
15 while the intervening region 64c is again apertured. Thus pockets or condensate collecting regions are formed under the end portions (in the circumferential direction) of the floor, in which pockets condensate may accumulate during rotation. In this modification, up to five condensate removal ports 67 may be provided so that condensate may be extracted or removed from the vessel 1 while the vessel 1 is in
20 motion or otherwise, both from beneath the "solid" false floor portions 64a, 64b and also from underneath the perforated liner portion 64c, either from the lowermost portion of the vessel, during vessel movement, under the action of gravity, or alternatively by being engaged against the inner side 48 of the outer wall of the vessel by centrifugal force. The ports 67 in the non-apertured floor region are optional. Thus, in this version
25 of the invention, the non-apertured floor regions define spaces in which condensate which collects or accumulates during rotation may be gathered or collected and held, at least temporarily, for a period during the process, for optional release at any selected time.

30 The remaining features of the construction of Figure 19 are in accordance with these of Figure 17.

Referring now to Figures 20 and 21, there is illustrated the provision of a lifting arrangement 51a, 51b and 51c as defined in accordance with the present invention within a steam peeling vessel 1' of known or substantially conventional construction. In this prior art pressure vessel, the unit 1' has a generally cylindrical form and is rotated about a transverse axis 7 perpendicular to the longitudinal axis of the vessel 1'. The door and loading and discharge point 4' are located at one axial end of this elongate vessel 1'. As shown in Figures 20 and 21, the vessel 1' is provided with a series of lifting features, 51a', 51b' and 51c' these being defined by indents or protrusions directed inwardly from the region of the inner wall 48' of the pressure vessel and defined, in the particular embodiment shown, by inward indentations or protrusions formed in a perforated condensate floor or liner 64' as described in connection with the vessel of Figures 17, 18 and 19. However, the provision of lifters 51a', 51b' and 51c' within this pressure vessel 1' of conventional or prior art design is not confined to arrangements in which they are formed by deformations of a condensate floor 64'. In variants of the invention, the inwardly directed lifters 51a', 51b' and 51c' may be defined by independent features, appropriately located on suitable regions of the inner wall 48' of the pressure vessel 1', such as welded on angled plate portions, as previously described, and the lifters 51a', 51b' and 51c' may then also define steam savers as understood in terms of the present invention.

The unit 1, 1' of the invention provides exceptionally good product mixing during steam treatment. Within the rotational speed range specified, not only is the degree of mixing good, but the mixing action is such that there is also minimal damage to product 3, for example potatoes or also small carrots. Even in the event of an extended mixing period, not usual in conventional operation, the level of damage is nonetheless minimised. The mixing action is such that products 3 such as potatoes or small carrots roll at all times and there is no throwing of product 3. The mixing action is directed to enabling steam to access each individual product 3, and this is facilitated by the tumbling action according to the system of the invention. The action provided by the present invention is to be distinguished from the stirring type mixing used in other technologies, where the objective is to effectively integrate or sift together a multiplicity

of different media. In the present invention, the objective is to give access for steam to the external surface of every product item 3 to an optimum extent.

Moving on now to the expansion chamber and steam discharge features of the system of the invention, Figure 22 shows the expansion chamber 21 of the invention, in one embodiment. Steam enters the expansion chamber 21 at valve 57 from the steam peeler pressure vessel 1 in the manner already described and the volume of the expansion chamber 21 is sufficient for very rapid reduction of pressure as the steam discharges into it. In order however to ensure the speediest possible final drop in pressure towards atmospheric at the end of the discharge cycle, the arrangement of Figure 22 also incorporates a water spray feature 68. A volume of water in a pressure vessel 69 for supply of spray water is pressurised by an air line or booster pump and is blown through water balls or spray heads 68 when the pressure in the blowdown pressure vessel 21 falls to a predetermined value. Release or discharge of this water into the expansion chamber 21 is regulated by a water release valve 71. A pressure regulator 72 controls the air pressure applied to the spherical pressure vessel 69 to ensure constant water pressure at the water balls 68. Water is sprayed in at the end of the blowdown cycle, when the pressure in the peeler pressure vessel 1 drops to approximately 0.3 bar. This ensures continued pull-down of pressure within the expansion chamber 21 towards the end of the discharge cycle, there being no difficulty in achieving rapid, effectively substantially instantaneous pressure drop at the start of the exhaust phase. In practice, the extremely rapid drop in pressure results in the water spray 68 becoming activated about 0.5 seconds into the discharge or pressure drop phase. The rapid expansion and accelerated reduction in pressure is further facilitated by use of a large diameter stack 28.

Other features of the arrangement are a sloping floor 73 to the expansion chamber 21, for collection of condensate at a sump 74, and a baffle 75 located between the steam entry point and the discharge duct or stack 28. Baffle 75 extends downwards at an acute angle from the roof of the chamber 21 towards the stack 28 region of the chamber 21 and terminates at a location where its free end region substantially underlies, at least in part, the exit point where steam leaves the chamber

21 and enters the stack 28. In order to reduce carryover of solids and/or odour to the external environment, a water trap 76 is provided at the top end of the stack, so that discharge vapours are bubbled through this water trap 76 before reaching atmosphere at outlet zone 77. In order to ensure that the discharge duct or stack 28 in no way
5 throttles the reduction of pressure in the expansion chamber 21, the stack 28 provides substantially greater cross-sectional flow area than prior art arrangements, typically greater by a factor of 4.

Figure 23 shows a further variant, in which the discharge stack 28 does not
10 exit directly from the expansion chamber 21 proper, but rather from a solids trap 78, defined by a hopper-type structure communicating with the expansion chamber 21 by way of a duct 79 of large dimensions. The stack 28, again of large cross-sectional area, exits from an upper region 81 of this solids trap, but has a downwardly projecting flange or extension 82 extending in part into the solids trap 78, so that
15 steam or vapour exiting from the expansion chamber 21 is required to follow a convoluted path from the upper stream entry region 81 of the solids trap 78 initially in a downwards direction, to turn around the edge of the downwardly projecting flange or extension 82 and then discharge upwards through the stack 28. In this way, a type of baffle structure is provided.

20

In all variants of the stack structure 28, it is preferred that a relatively tall or elongated stack structure 28 be used in conjunction with the odour containment and solids trapping features of the invention.

25 The words "comprises/comprising" and the words "having/including" when used herein with reference to the present invention are used to specify the presence of stated features, integers, steps or components but does not preclude the presence or addition of one or more other features, integers, steps, components or groups thereof.

Claims

1. A pressure vessel for steam treatment of product to be peeled in a steam peeling system, the pressure vessel having substantially the shape of a sphere with
5 opposed flattened side surfaces.
2. A pressure vessel according to Claim 1, wherein the pressure vessel is defined at least in part by two opposed dish-shaped portions engaged together along rim regions of the portions to define an enclosed interior region.
10
3. A pressure vessel according to Claim 1, wherein the pressure vessel is defined at least in part by two opposed dish-shaped portions welded together rim to rim to define an enclosed interior region.
- 15 4. A pressure vessel according to any preceding claim, wherein the aspect ratio between a maximum diameter of the pressure vessel and a dimension of the pressure vessel between the opposed flattened side surfaces is greater than about 1.2:1.
5. A pressure vessel according to Claim 4, wherein the aspect ratio is about 2:1.
20
6. A pressure vessel according to any preceding claim, wherein the pressure vessel is substantially symmetrical at least about an axis extending between the opposed flattened side surfaces of the pressure vessel.
- 25 7. A pressure vessel according to Claim 6, wherein the pressure vessel is rotatable about said axis of substantial symmetry.
8. A steam peeling system comprising a pressure vessel according to any of Claims 1 to 7.
30
9. A pressure vessel for steam treatment of product to be peeled in a steam peeling system, the pressure vessel being rotatable and having at least one internal

lifting feature for entraining and raising product relative to the axis of rotation of the pressure vessel during rotation of the pressure vessel.

10. A pressure vessel according to any of Claims 1 to 8, wherein the pressure
5 vessel has at least one internal lifting feature for entraining and raising product relative to the axis of rotation of the pressure vessel during rotation of the pressure vessel.

11. A pressure vessel according to Claim 9 or Claim 10, wherein the or each
10 internal lifting feature comprises a protrusion extending inwards from the region of an interior surface of a wall portion of the pressure vessel, substantially in the direction of the axis of rotation of the vessel.

12. A pressure vessel according to Claim 11, wherein the or each internal lifting
15 feature extends substantially radially inwards.

13. A pressure vessel according to Claim 11 or Claim 12, wherein the or each
internal lifting feature extends directly from the interior wall surface of the wall portion of the pressure vessel.

20 14. A pressure vessel according to Claim 11 or Claim 12, wherein the or each internal lifting feature is defined by an upstanding portion of a false floor which is spaced from the interior wall surface of the wall portion of the pressure vessel.

15. A pressure vessel according to Claim 14, wherein at least a portion of the
25 false floor is apertured for the passage of condensate through the apertures of the false floor during use of the system, for accumulation of condensate in the region between the false floor and the interior wall surface of the wall portion of the pressure vessel.

16. A pressure vessel according to Claim 15, wherein at least a portion of the
30 false floor is non-apertured to provide a region for at least temporary retention of condensate accumulating during rotation of the vessel.

17. A pressure vessel according to Claim 15 or Claim 16, wherein the pressure vessel is provided with means for enabling removal of condensate from the region between the false floor and the interior wall surface of the wall portion of the pressure
5 vessel during operation of the system.

18. A pressure vessel according to any of Claims 9 to 13, wherein the or each internal lifting feature defines a closed region which is not in communication with the remainder of the interior space within the pressure vessel for the movement of gas or
10 vapour between the closed region and the remainder of the interior space within the pressure vessel.

19. A steam peeling system comprising a pressure vessel according to any of Claims 9 to 18.
15

20. A pressure vessel for steam treatment of product to be peeled in a steam peeling system, the pressure vessel having at least one internal region which is closed-off against ingress of steam during product treatment, said region defining a steam
20 saver.

21. A pressure vessel according to any of Claims 1 to 7, wherein the pressure vessel has at least one internal region which is closed-off against ingress of steam during product treatment, said region defining a steam saver.

22. A pressure vessel according to Claim 20 or Claim 21, wherein said at least one internal region is defined within an enclosure, all portions of which are spaced apart from any interior wall surface of the pressure vessel.
25

23. A pressure vessel according to Claim 20 or Claim 21, wherein the pressure
30 vessel is rotatable and said at least one internal region which is closed-off against ingress of steam during product treatment is defined by an internal lifting feature for

entraining and raising product relative to the axis of rotation of the pressure vessel during rotation of the pressure vessel.

24. A pressure vessel according to Claim 23, wherein said internal lifting feature
5 is provided in accordance with any of Claims 11 to 14.

25. A pressure vessel according to Claim 20 or Claim 21, wherein said at least
one internal region which is closed-off against ingress of steam during product treatment
is provided on the side of a door of the pressure vessel, which side is directed towards
10 the interior of the vessel.

26. A pressure vessel according to Claim 20 or Claim 21, wherein said at least
one internal region which is closed-off against ingress of steam during product treatment
is provided by an enclosure located on a wall portion of the vessel in the vicinity of an
15 axis of symmetry of the vessel.

27. A pressure vessel according to Claim 26, wherein said enclosure is
symmetrically located with respect to the said axis of symmetry of the vessel.

20 28. A steam peeling system comprising a pressure vessel according to any of
Claims 20 to 27.

29. A rotary product batching unit comprising a plurality of compartments
arranged for advancing movement within an enclosing housing, for selective
25 successive alignment of each compartment with a product loading location and
subsequent alignment of the compartment with a product discharge location.

30. A rotary product batching unit according to Claim 29, wherein each
compartment of the batching unit is defined between radially spaced apart and radially
30 extending blades of vanes mounted for rotation about a common axis.

31. A rotary product batching unit according to Claim 29 or Claim 30, wherein the batching unit is mounted by way of weighing means, for computation of the weight of product accommodated by the batching unit.
- 5 32. A rotary batching unit according to Claim 31, wherein said weighing means comprises a plurality of load cells.
33. A steam peeling system comprising a rotary batching unit for cooperation with a pressure vessel for steam treatment of product to be peeled, the rotary batching
10 unit having a plurality of compartments arranged for advancing movement within an enclosing housing, for selective successive alignment of each compartment with a product loading location and subsequent alignment of the compartment with a location for discharge of product to the pressure vessel.
- 15 34. A steam peeling system according to any of Claims 8, 19 and 28, comprising a rotary batching unit for cooperation with the pressure vessel, the rotary batching unit having a plurality of compartments arranged for advancing movement within an enclosing housing, for selective successive alignment of each compartment with a product loading location and subsequent alignment of the compartment with a location
20 for discharge of product to the pressure vessel.
35. A steam peeling system according to Claim 33 or Claim 34, wherein each compartment of the batching unit is defined between radially spaced apart and radially extending blades or vanes mounted for rotation about a common axis.
25
36. A steam peeling system according to any of Claims 33 to 35, wherein the batching unit is mounted by way of weighing means, for computation of the weight of product accommodated by the batching unit.
- 30 37. A steam peeling system according to claim 36, wherein said weighing means comprises a plurality of load cells.

38. A steam peeling system comprising a pressure vessel for steam treatment of product to be peeled and an expansion chamber for receiving pressurised steam discharged from the pressure vessel at the end of a steam treatment phase of a steam peeling operation, means being provided for enabling release of pressurised steam from the pressure vessel into the expansion chamber, said means being located substantially at the point of entry of steam into the expansion vessel.

39. A steam peeling system according to any of Claims 8, 19, 28 and 33 to 37, comprising an expansion chamber for receiving pressurised steam discharged from the pressure vessel at the end of a steam treatment phase of a steam peeling operation, means being provided for enabling release of pressurised steam from the pressure vessel into the expansion chamber, said means being located substantially at the point of entry of steam into the expansion vessel.

40. A steam peeling system according to Claim 38 or Claim 39, wherein the cross-sectional flow area of the pressure releasing means increases progressively through said means from an inlet region of the pressure releasing means to a discharge region of the means.

41. A steam peeling system according to Claim 40, wherein said pressure releasing means comprises a valve.

42. A steam peeling system comprising a pressure vessel for steam treatment of product to be peeled, wherein pressurised steam is discharged from the pressure vessel through a port of the vessel at the end of a steam treatment phase of a steam peeling operation and the ratio between pressure vessel volume in litres and the area of said port in square inches is less than about 20:1.

43. A steam peeling system according to any of Claims 8, 19, 28, and 33 to 40, wherein pressurised steam is discharged from the pressure vessel through an exhaust port of the vessel at the end of a steam treatment phase of a steam peeling operation and

the ratio between pressure vessel volume in litres and the area of said port in square inches is less than about 20:1.

44. A steam peeling system according to Claim 42 or Claim 43, wherein said
5 port comprises the only steam exhaust port from the pressure vessel.

45. A steam peeling system according to Claim 44, wherein said pressure vessel
comprises a single steam entry port.

10 46. A steam peeling system according to any of Claims 42 to 45, wherein steam
entry and steam exhaust takes place through said port.

47. A steam peeling system according to any of Claims 42 to 46, wherein said
ratio is in the range 10:1 to 20:1.

15

48. A steam peeling system according to any of Claims 42 to 47, wherein said
ratio is about 14:1.

49. A steam peeling system comprising a pressure vessel for steam treatment
20 of product to be peeled and an expansion chamber for receiving pressurised steam
discharged from the pressure vessel at the end of a steam treatment phase of a steam
peeling operation, means being provided for release of steam and/or vapour from the
expansion chamber to atmosphere, said means comprising an arrangement for
substantially minimising release of entrained solid matter and/or odours in steam
25 and/or vapour leaving the expansion chamber.

50. A steam peeling system according to any of Claims 8, 19, 28 and 33 to 48,
comprising means for release of steam and/or vapour from to atmosphere from an
expansion chamber for receiving pressurised steam discharged from the pressure vessel
30 at the end of a steam treatment phase of a steam peeling operation, said means
comprising an arrangement for substantially minimising release of entrained solid
matter and/or odours in steam and/or vapour leaving the expansion chamber.

51. A steam peeling system according to Claim 49 or Claim 50, wherein a baffle is located within the expansion chamber and a solids trap is located substantially at the exit location from a stack communicating between the interior of the expansion chamber
5 and atmosphere.

52. A steam peeling system according to Claim 49 or Claim 50, wherein a solids trap is located in the interior of the expansion chamber.

10 53. A steam peeling system comprising a control system for regulating movements of a pressure vessel for steam treatment of product to be peeled between loading and discharge dispositions of the pressure vessel through a succession of treatment stages, unproductive displacement of the pressure vessel being substantially minimised during said movements.

15

54. A steam peeling system according to any of Claims 8, 19, 28 and 33 to 52, comprising a control system for regulating movements of the pressure vessel between loading and discharge dispositions of the pressure vessel through a succession of treatment stages, unproductive displacement of the pressure vessel being substantially
20 minimised during said movements.

55. A steam peeling system according to Claim 53 or Claim 54, wherein the control system provides for discharge of product from the pressure vessel while the vessel is in motion during a treatment/process cycle.

25

56. A steam peeling system according to any of Claims 53 to 55, wherein the control system provides for opening and/or closing of a door portion of the pressure vessel while the vessel is in motion during a treatment/process cycle.

30 57. A steam peeling system according to any of Claims 53 to 56, wherein the pressure vessel is rotatable.

58. A steam peeling system according to Claim 57, wherein the control system provides for reversal of the direction of rotation of the pressure vessel during a treatment/process cycle.
59. A steam peeling system according to Claim 58, wherein the direction of rotation during dump or discharge of product from the pressure vessel is opposite to the direction of rotation of the pressure vessel at the start of treatment/process cycle.
60. A steam peeling system according to any of Claims 53 to 59, wherein the control system provides variation of speed of movement of the pressure vessel during a treatment/process cycle.

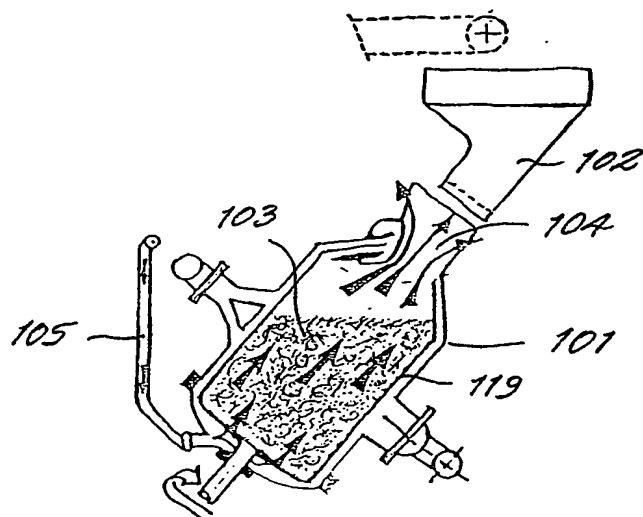


Fig. 1

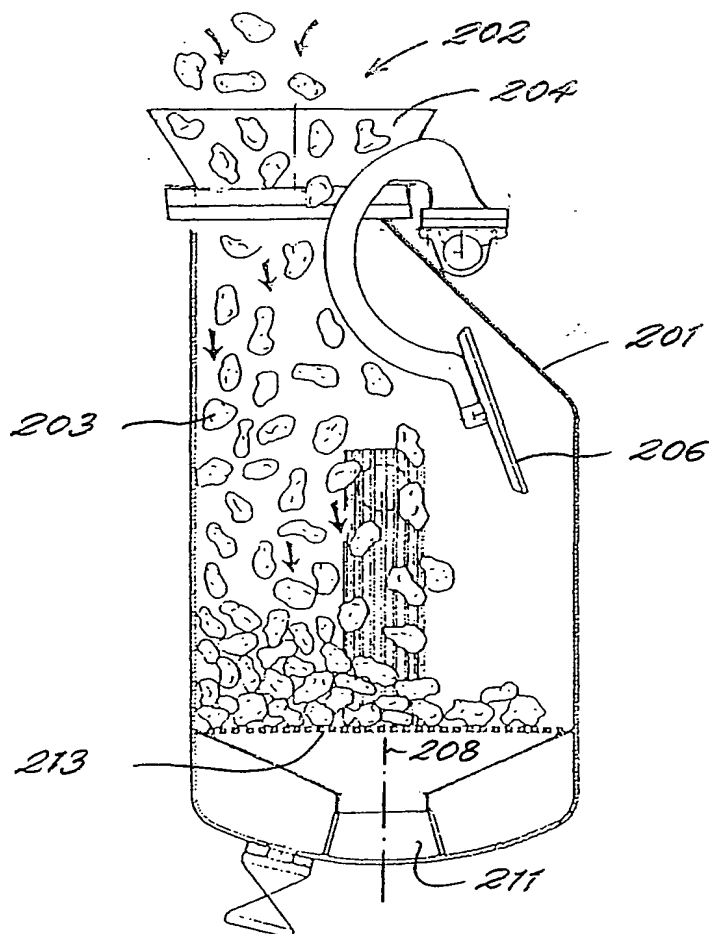
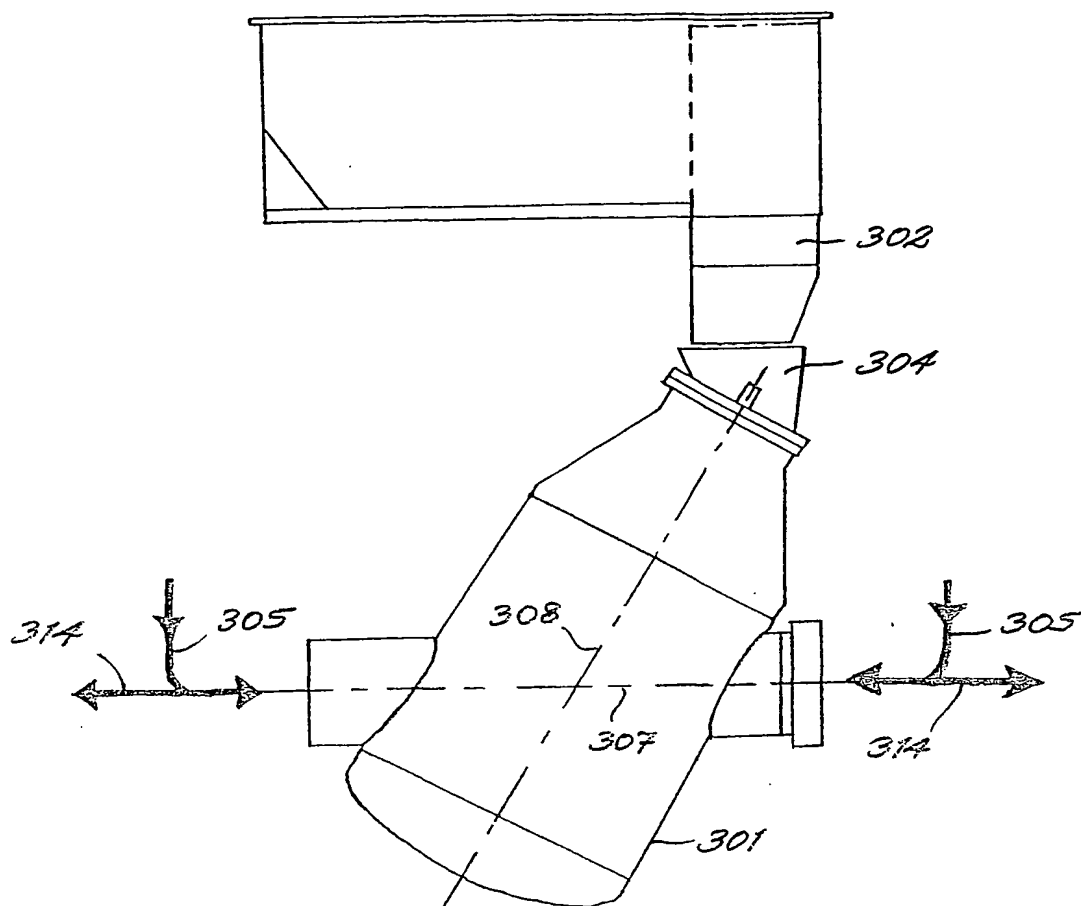
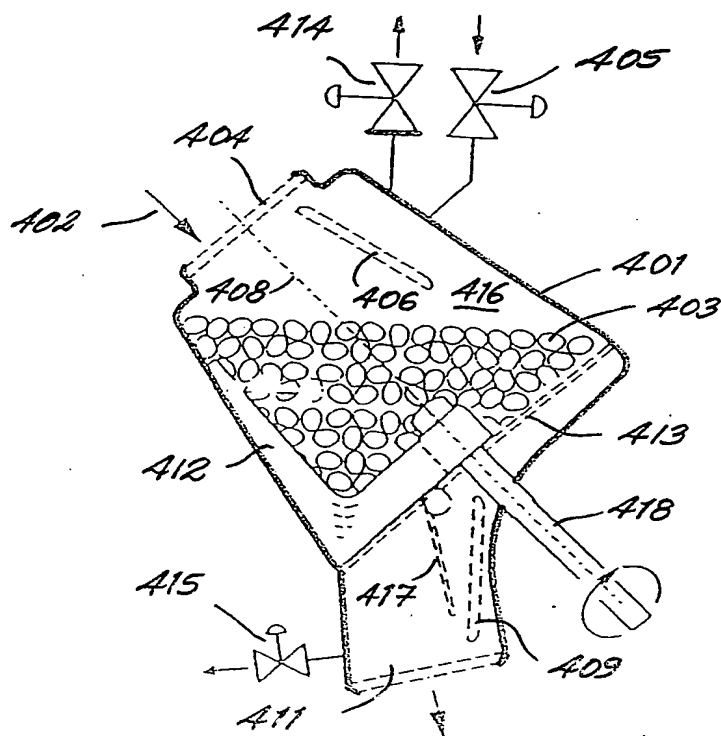
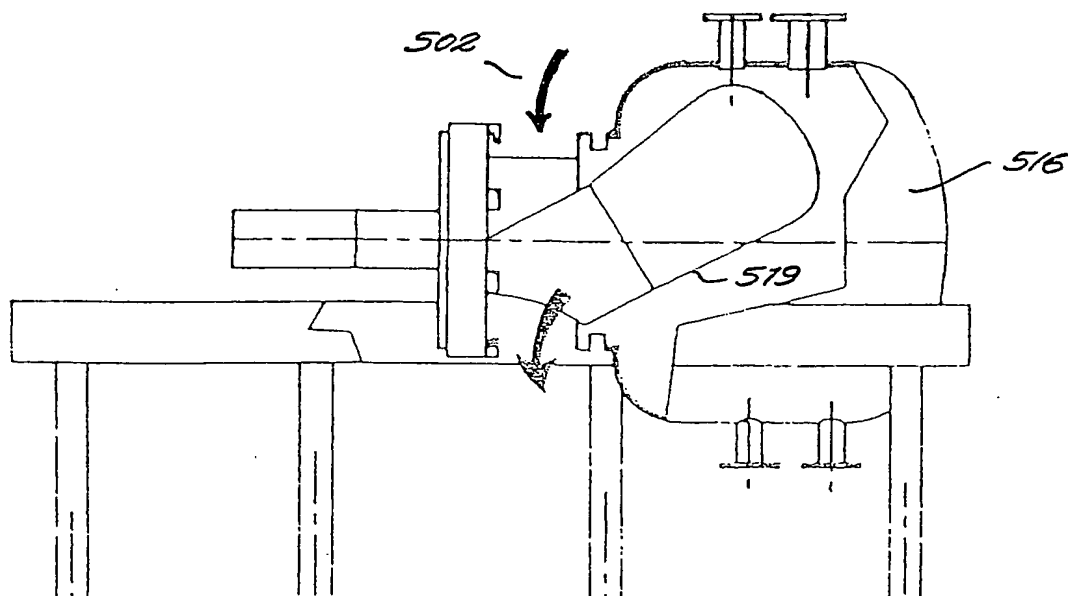


Fig. 2

**Fig. 3**

**Fig. 4****Fig. 5**

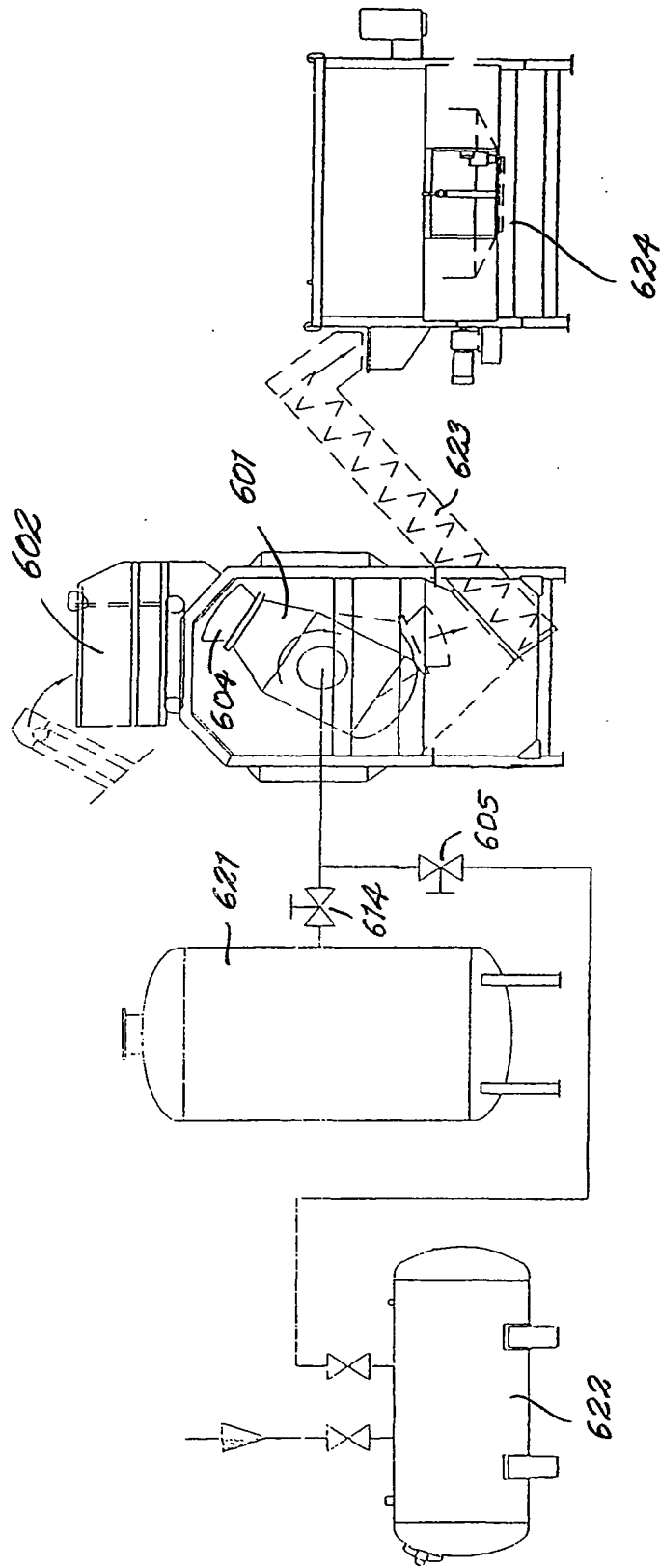


Fig. 6

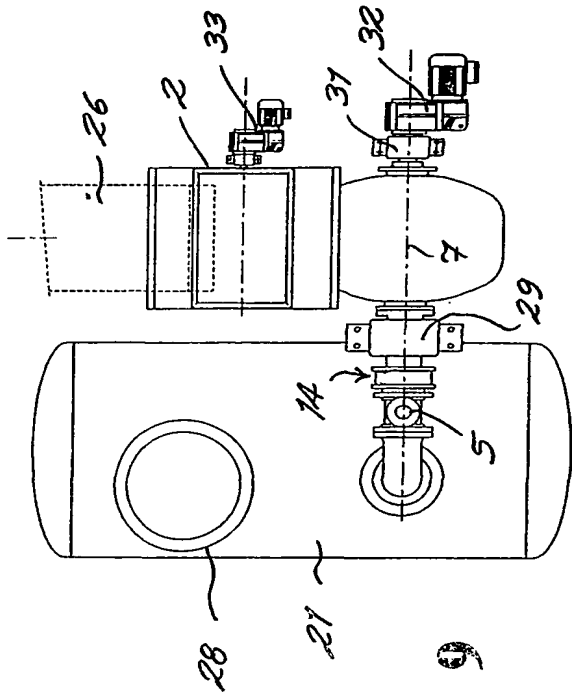


Fig. 9

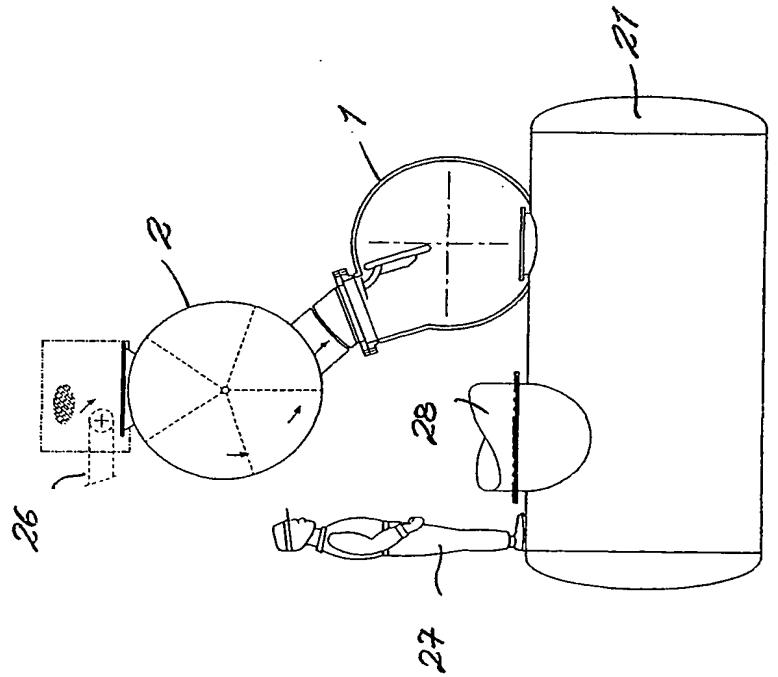


Fig. 7

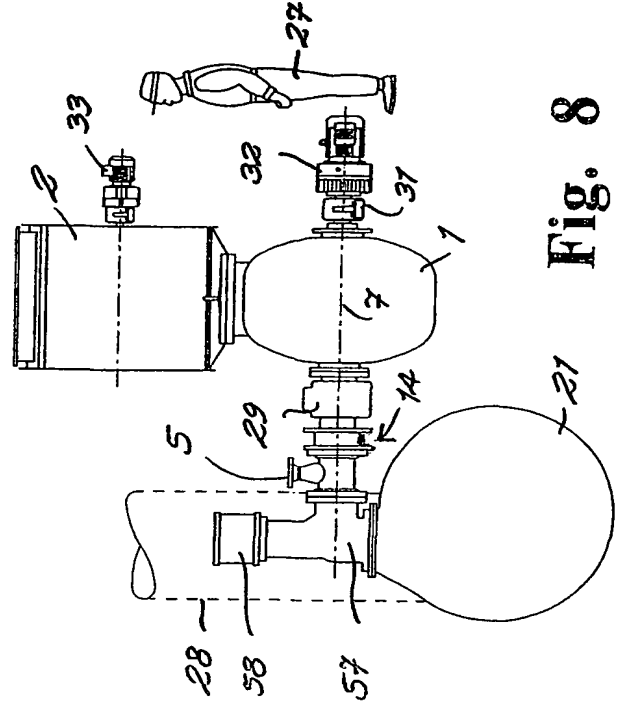


Fig. 8

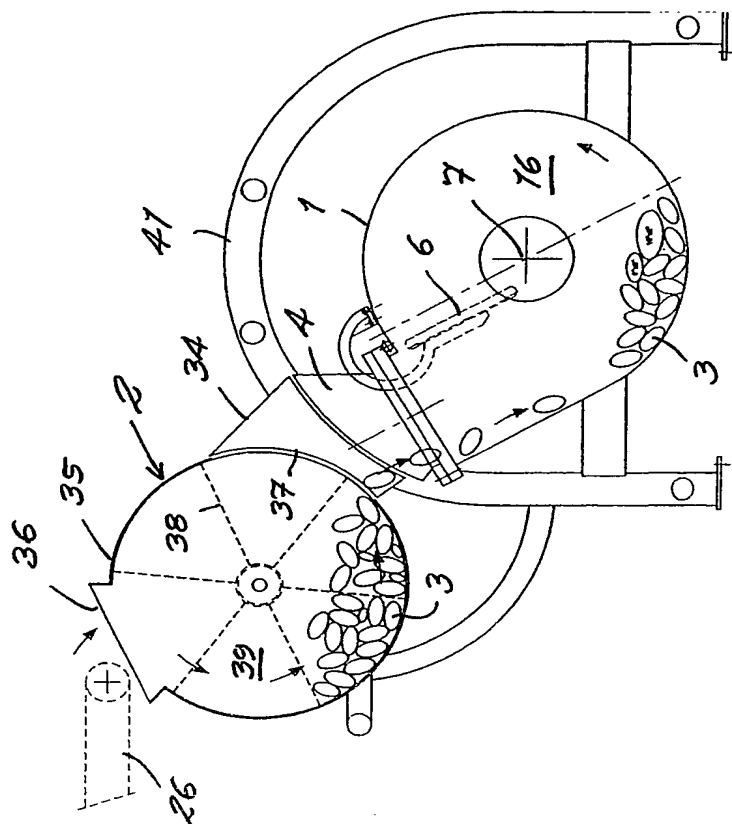


Fig. 10

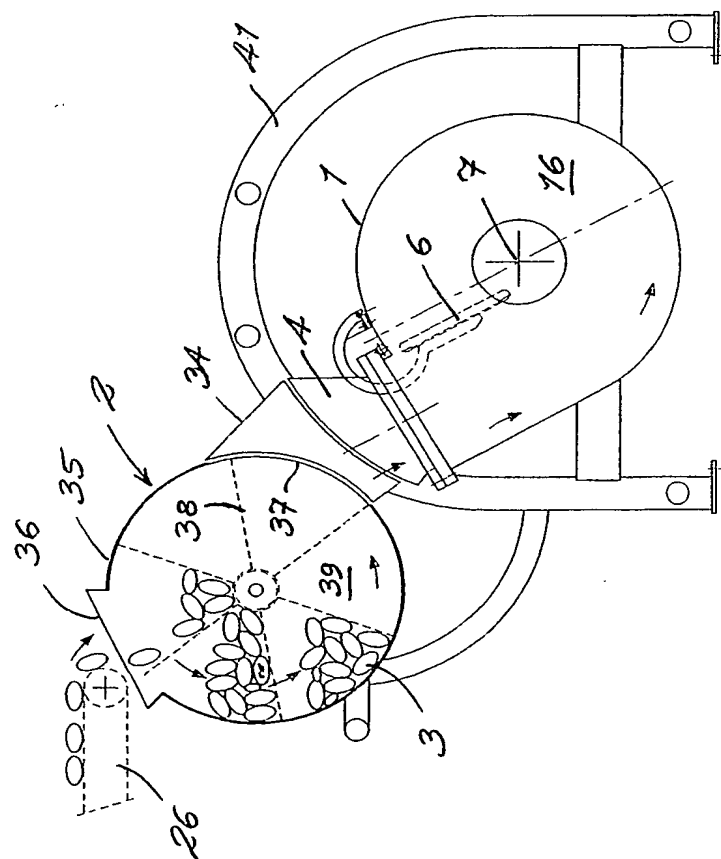


Fig. 11

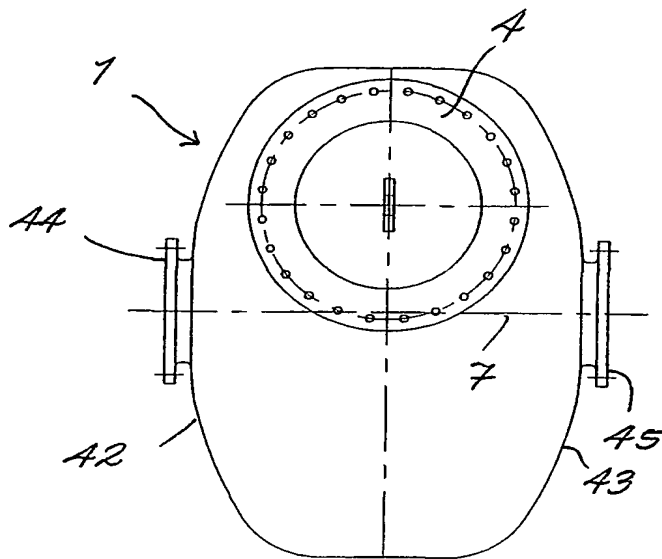


Fig. 14

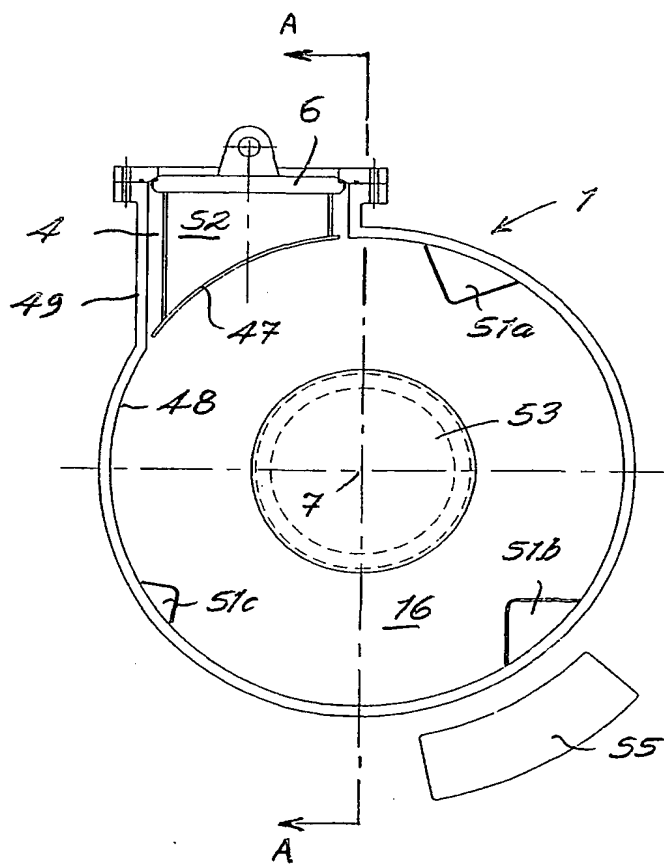


Fig. 12

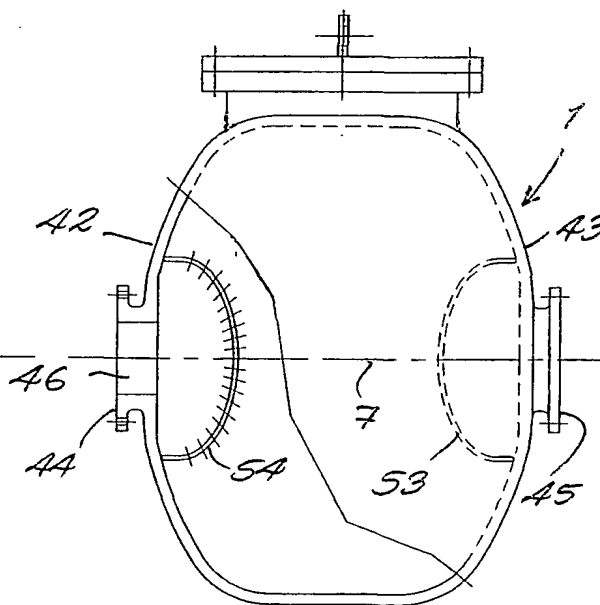


Fig. 13

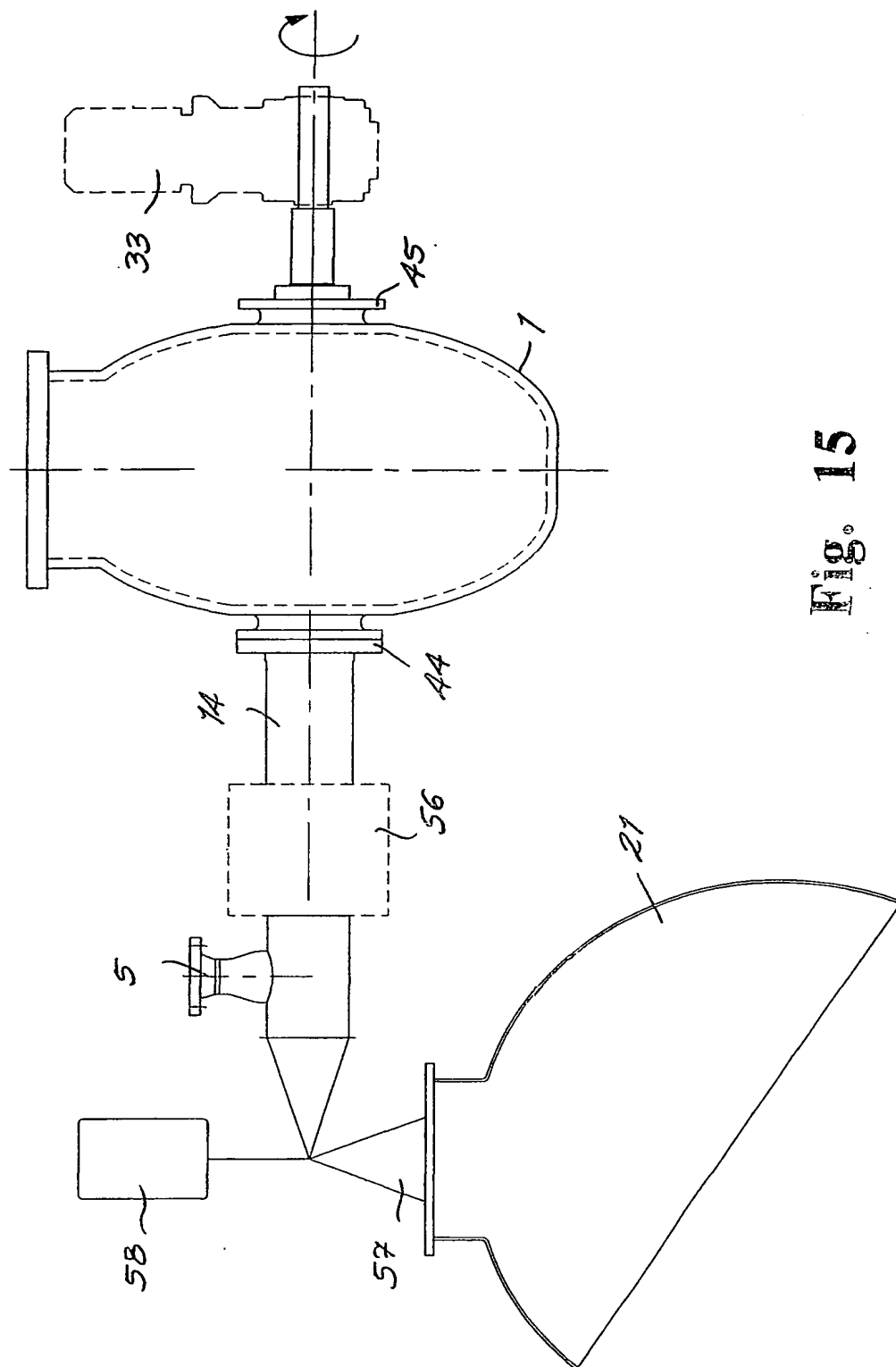


Fig. 15

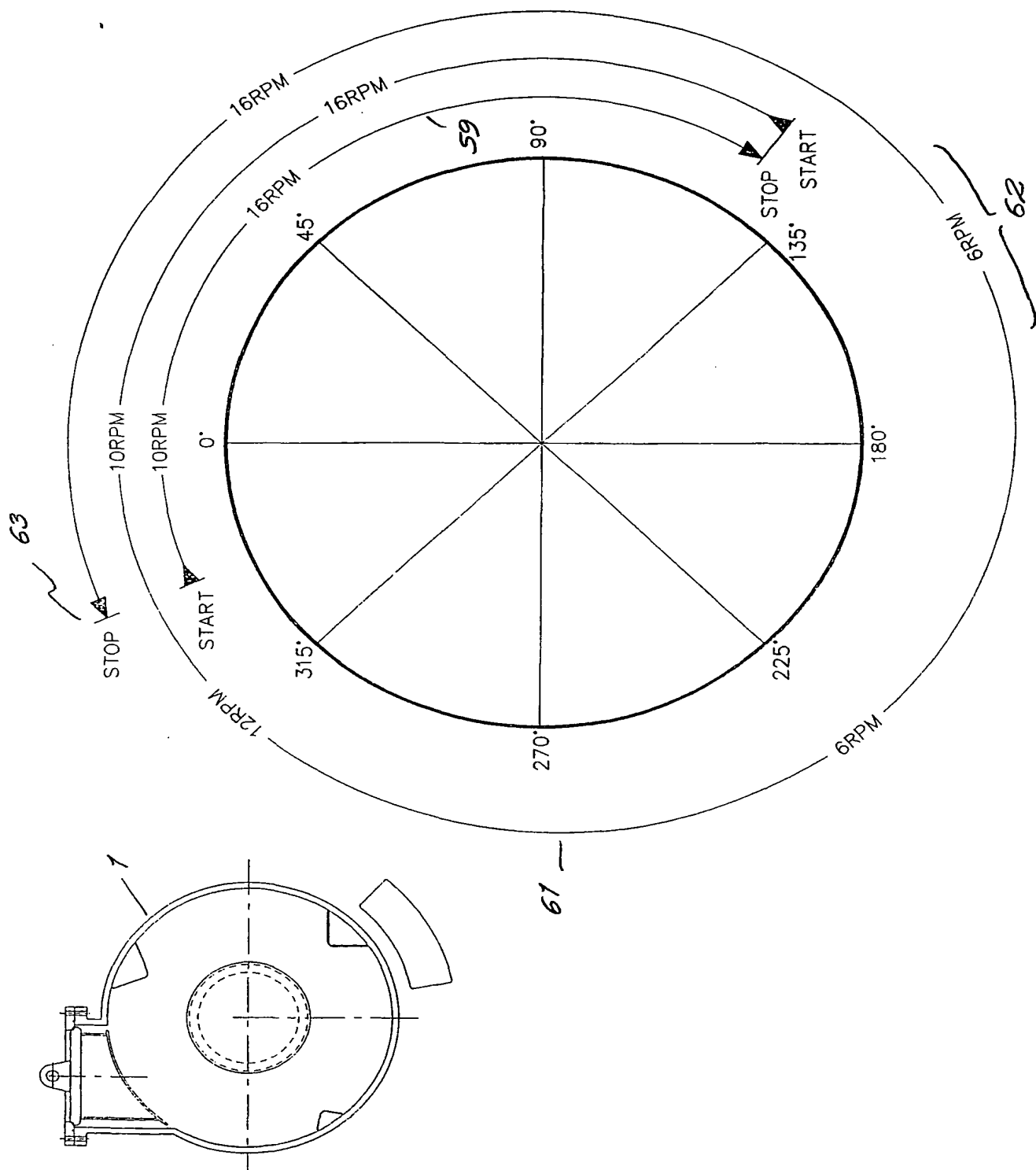


Fig. 16

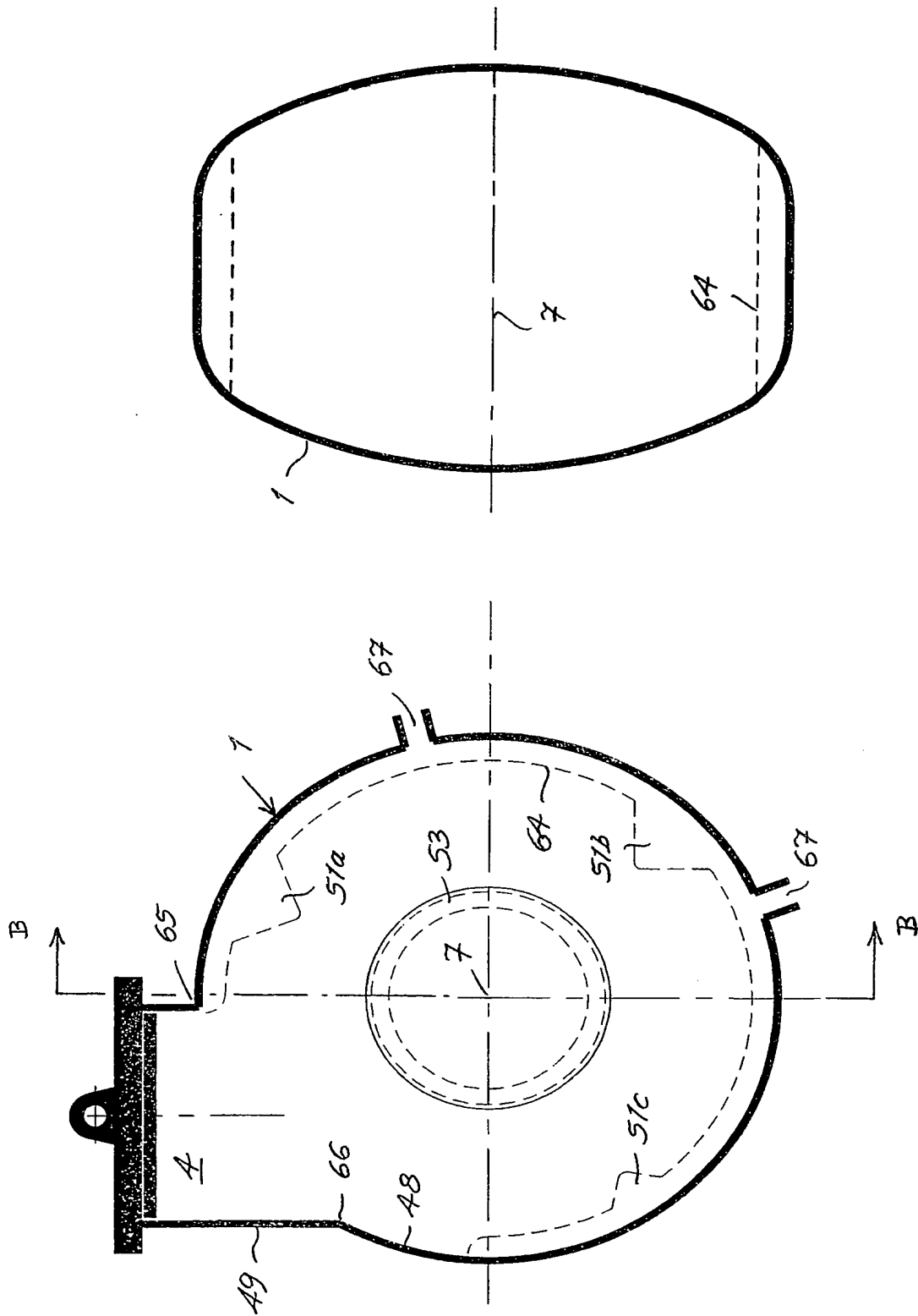


Fig. 18

Fig. 17

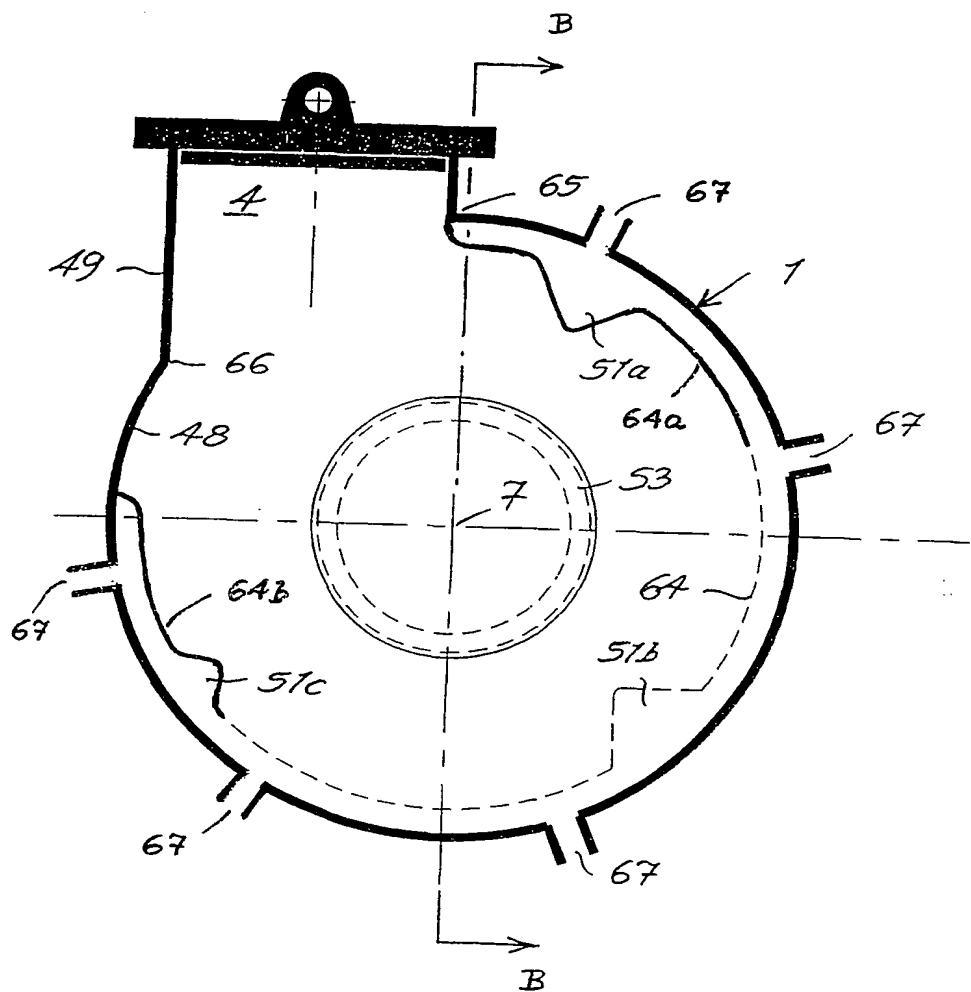


Fig. 19

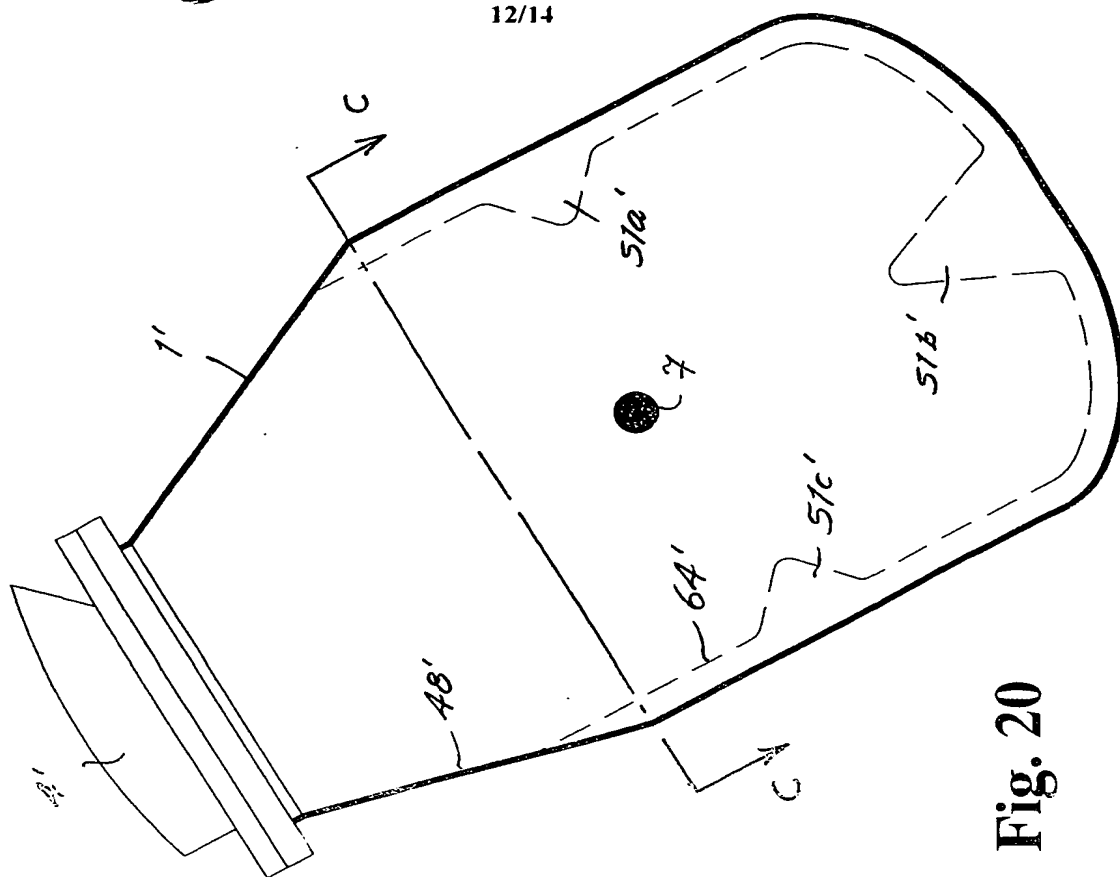


Fig. 20

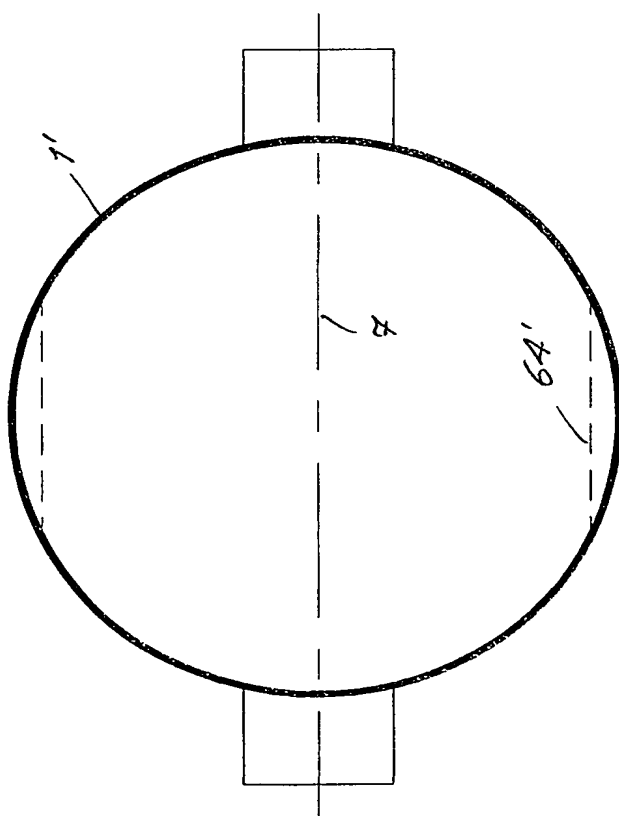


Fig. 21

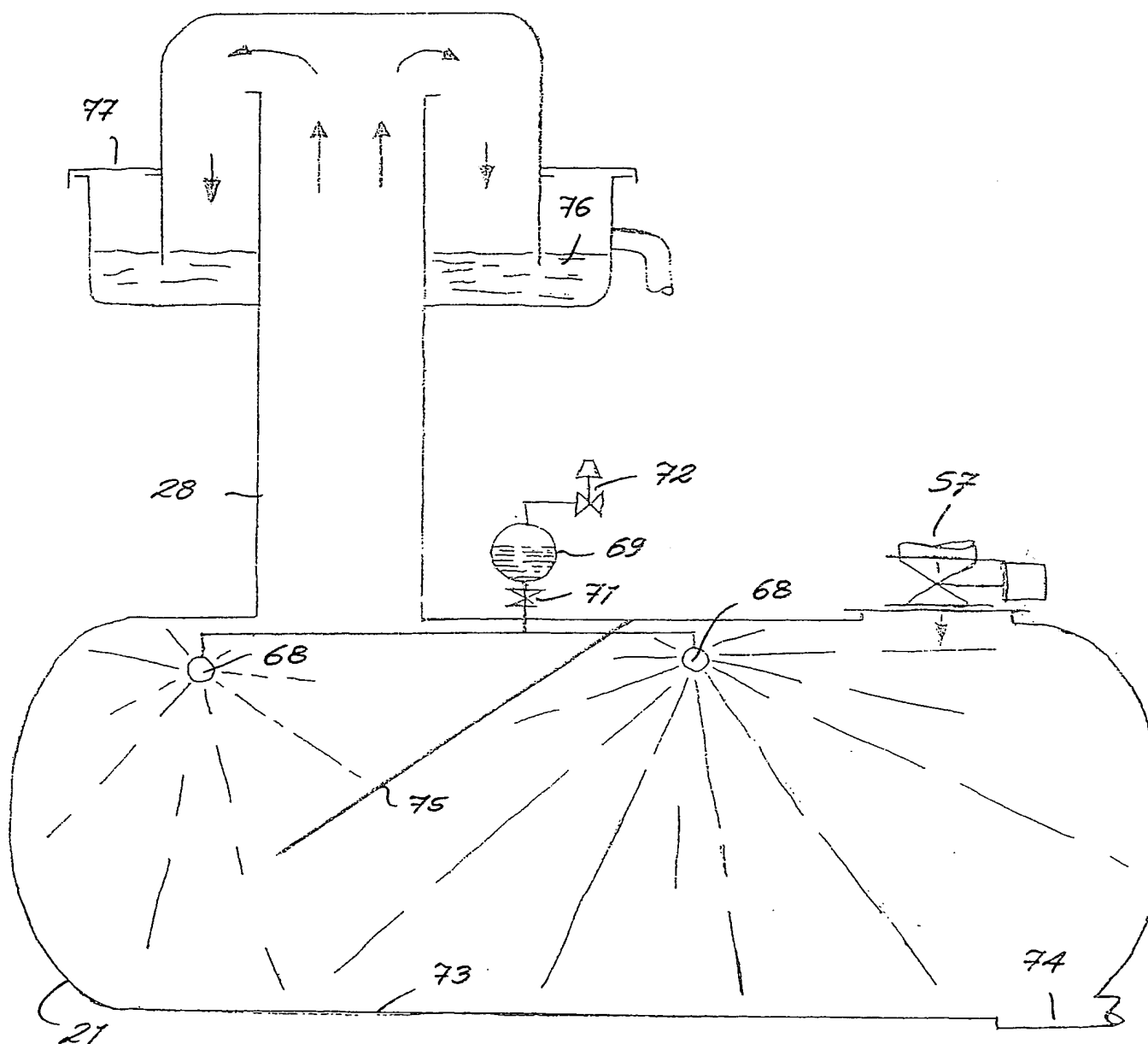
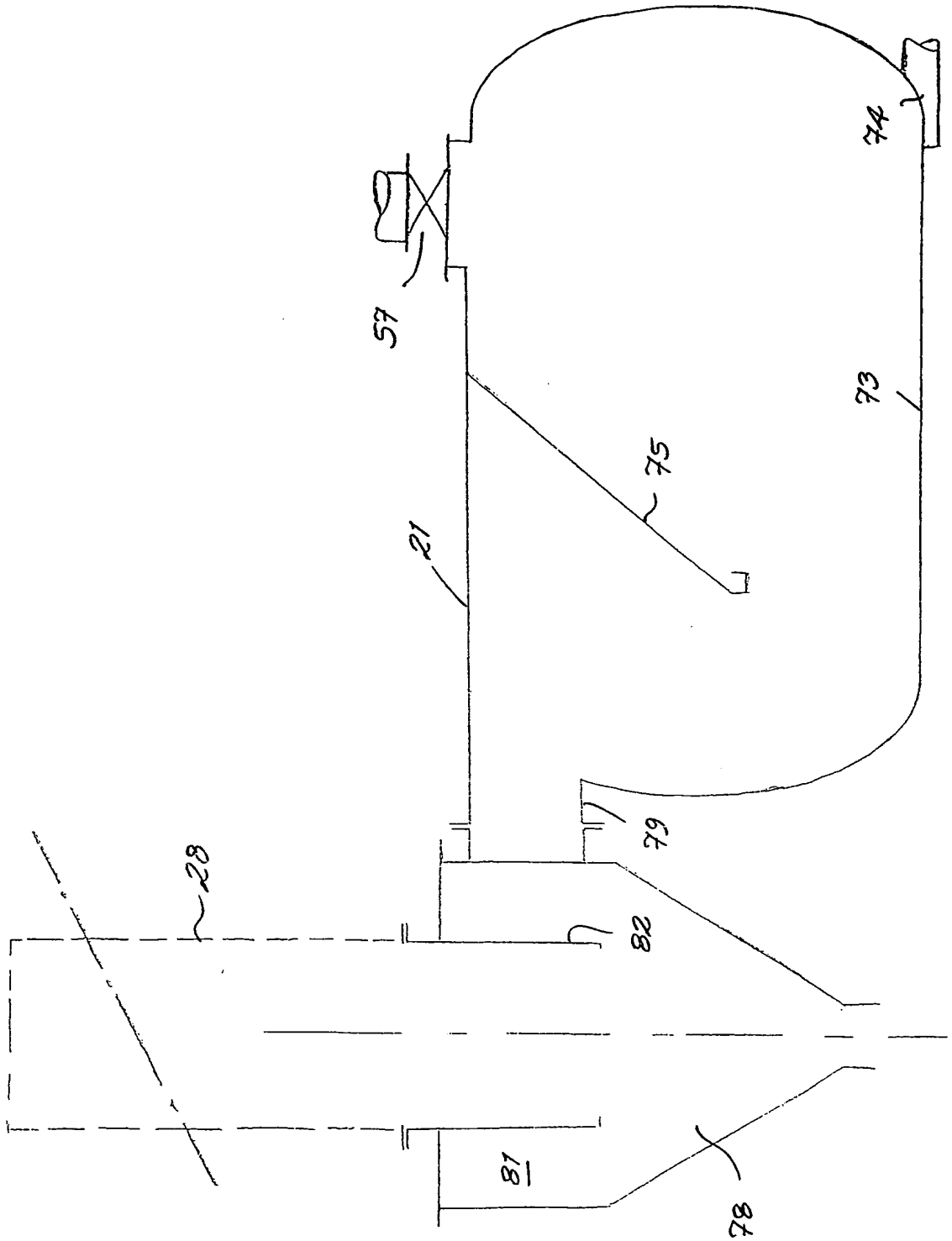


Fig. 22



INTERNATIONAL SEARCH REPORT

In **International Application No**
PCT/IE 01/00076

A. CLASSIFICATION OF SUBJECT MATTER

IPC 7 A23N7/00

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 7 A23N

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

EPO-Internal, PAJ, WPI Data

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X Y A	GB 2 247 829 A (OSENEY LTD) 18 March 1992 (1992-03-18) page 9, line 2 - line 6, paragraph 1 page 9, paragraph 3 -page 13, paragraph 2 page 14, paragraph 3 -page 16, paragraph 1 figures 2,3 --- -/--	53 31-33, 35-37 1,8,9, 19,20, 38,39, 42,49, 55,56,60



Further documents are listed in the continuation of box C.



Patent family members are listed in annex.

* Special categories of cited documents :

- *A* document defining the general state of the art which is not considered to be of particular relevance
- *E* earlier document but published on or after the international filing date
- *L* document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)
- *O* document referring to an oral disclosure, use, exhibition or other means
- *P* document published prior to the international filing date but later than the priority date claimed

T later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

X document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

Y document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.

8 document member of the same patent family

Date of the actual completion of the international search

21 September 2001

Date of mailing of the international search report

01/10/2001

Name and mailing address of the ISA

European Patent Office, P.B. 5818 Patentlaan 2
NL - 2280 HV Rijswijk
Tel. (+31-70) 340-2040, Tx. 31 651 epo nl,
Fax: (+31-70) 340-3016

Authorized officer

Amaro, H

INTERNATIONAL SEARCH REPORT

In onal Application No
PCT/IE 01/00076

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	AT 367 982 B (SCHUG PETER ; SCHUG FRIEDRICH (DE); SCHUG HANS (DE)) 25 August 1982 (1982-08-25)	29, 30
Y	page 4, line 37 - line 41 figure 2	31-33, 35-37
X	US 4 707 372 A (CATELLI CAMILLO) 17 November 1987 (1987-11-17)	29, 30
A	column 2, line 46 - line 51	31-37
A	FR 2 213 741 A (FLORIGO APP BV) 9 August 1974 (1974-08-09) page 1, line 1 - line 10 page 4, line 22 - line 28 figure 1	1, 8, 9, 19
A	GB 1 454 119 A (KIREMKO BV) 27 October 1976 (1976-10-27) claims 1, 6, 7 figure 1	1, 8, 9, 19

INTERNATIONAL SEARCH REPORT

Information on patent family members

International Application No

PCT/IE 01/00076

Patent document cited in search report		Publication date	Patent family member(s)	Publication date
GB 2247829	A	18-03-1992	BE 1003969 A6 LU 87835 A1	28-07-1992 07-05-1991
AT 367982	B	25-08-1982	AT 364236 B AT 780678 A AT 21278 A	12-10-1981 15-01-1982 15-02-1981
US 4707372	A	17-11-1987	IT 1187158 B	16-12-1987
FR 2213741	A	09-08-1974	NL 7300503 A DE 2330662 A1 FR 2213741 A1 HU 165922 B	16-07-1974 18-07-1974 09-08-1974 28-12-1974
GB 1454119	A	27-10-1976	NL 7303774 A BE 811743 A1 DE 2409135 A1 FR 2222031 A1	23-09-1974 17-06-1974 03-10-1974 18-10-1974